

Computer Controlled Systems

- Course outline

- Wk 1: Introduction, Matlab and Simulink, PC104 platform, System simulation and Real-Time applications (Notes)
- Wk 2: Computer Interfacing for Data Acquisition and Control, ADC-DAC, Signal conditioning, quantization (Notes)
- Wk 3: Review of Z-transform and State Variables (Ch.2)
- Wk 4: Z-transform and state variables, Linearization (Ch.2)
- Wk 5: Sampling and Reconstruction, CT-DT conversions, Discretization (Ch.3, Notes)
- Wk 6: Discretization, Open-loop DT systems (Ch.4, Notes)
- Wk 7: Closed-Loop systems, Time/Frequency response characteristics (Notes, Ch. 5,6)
- Wk 8-9: Feedback and Feedforward Control, Stability Analysis, Nyquist/Bode (Notes, Ch. 7)
- Wk 10: PID controllers and tuning (Notes, Ch.8: Specs, PID)
- Wk 11: PID tuning and Controller Discretization (Notes)
- Wk 12: Feedforward Compensation (Notes)
- Wk 13: State Estimation (Ch.9: Observers)
- Wk 14: Model Identification (Notes, Ch. 10)
- Wk 15: Sensors, Actuators (Notes)

- (rev 9/2/15)

Introduction: The PC-104 Standard

- Low-power, general-purpose embedded applications
- Standard (small) size, stackable
 - Sound, PCMCIA, GPS, additional LAN, ADC-DAC,+...
- Advantech's PCM 3350
 - Stable geode processor (Pentium 300Mhz), on-chip PCI VGA, Intel82559 ER high performance Ethernet chip
 - 2 RS-232 serial ports
 - 128M RAM and FLASH memory (replacing the hard drive)

Introduction: The PC-104 Standard

- MATLAB compatibility: supported Ethernet chip for fast code download and testing.
 - Not crucial; one serial port can satisfy MATLAB's requirement for a comm. link; but communication is very slow and the port is lost to the application.
 - *check details in the web (advantech.com)*
- Operating system: DOS or Windows (CE).
 - DOS suffices for downloading MATLAB's real-time kernel and application program



Introduction: The PC-104 Standard

- Data acquisition and Control board: Diamond MM
 - Analog-to-Digital Conversion (ADC or A/D): 16 single ended or 8 differential analog inputs, 12-bit resolution, 2kHz software, 20kHz interrupt routine, 100kHz in DMA operation
 - Digital-to-Analog Conversion (DAC or D/A): 2 analog outputs, 12-bit resolution
 - 16 digital I/O lines (8 in, 8 out)
 - MATLAB compatibility: important to obtain quick results; but it offers only partial access to the board functions
 - [web page: diamondsystems.com](http://diamondsystems.com)

Introduction to Computers



- Microprocessor, motherboard, memory
 - address, data, control buses
 - CPU: Arithmetic Logic Unit, Accumulator, Program Counter, Instruction Register, Condition Codes Register, Control Unit, Clock speed, MIPS, FLOPS
 - TPA (Transient Program Area): operating system, Commands, I/O, BIOS, Interrupt vector
 - XMS (Extended Memory System)

Introduction to Computers

- Memory characteristics (older data)

| TYPE | AVG. CAPAC. | AVG. ACCESS | REL. COST |
|------------------|----------------|----------------|--------------|
| Cache | 0.5M | 2ns | 10 |
| Main | 50M | 20ns | 1 |
| Hard Disk | 50G | 10ms | 10^{-2} |
| Floppy Disk | 10M | 500ms | 10^{-3} |
| Magnetic Tape | 5G | 25s | 10^{-3} |
| CDROM | 600M | 500ms | 10^{-4} |
| DVDROM | 8G | 500ms | 10^{-5} |

Introduction to Computers



- I/O interfaces
 - isolated (IN-OUT instructions) and memory-mapped I/O
- Communication with external devices
 - polling: checking each device for service periodically (simple but inefficient)
 - interrupts: each device generates an interrupt that is serviced according to its priority level, in case of simultaneous arrivals

Introduction to Computers

- Arithmetic Computations (7 x 6, 7/2)
 - Integer:
 - $0111 \times 0110 = 01110 + 011100 = 101010$
 - $0111 / 0010 = (011.1) = 011$
 - Answer length increases by one bit in additions and one word in multiplications. Scaling and truncation is necessary for fixed word lengths
 - Floating point: (binary 5e3 format)
 - $0.11100e011 \times 0.11000e011 = (0.01110 + 0.00111)e\{011+011\} = 0.10101e110$
 - $0.111e011 / 0.100e010 = (1.11)e\{011-010\} = 0.111e010$

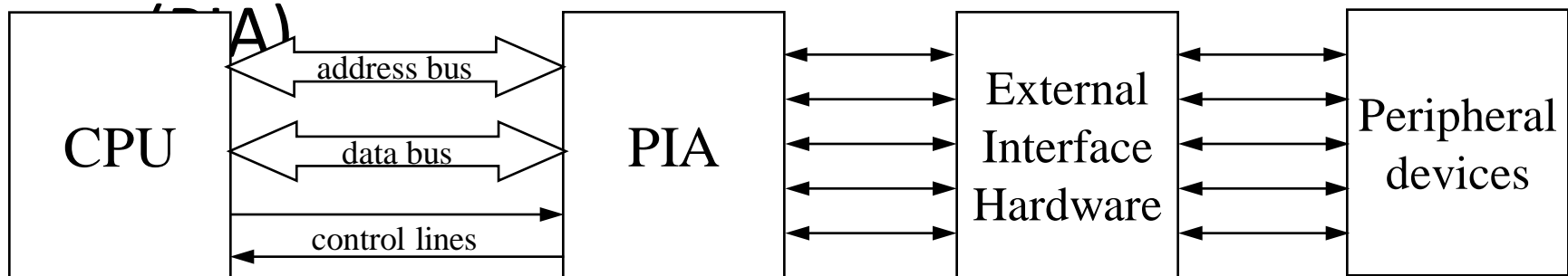
Introduction to Computers



- Math coprocessors perform a large variety of arithmetic operations (+, -, x, /, sqrt, sin, log, ...)
 - fast and high precision
 - hardware implementation of operations
 - computation uses algorithms and look-up tables
 - Newer CPUs have a built-in math coprocessor; nowadays, they are only absent in very-low-cost, or very-fast applications

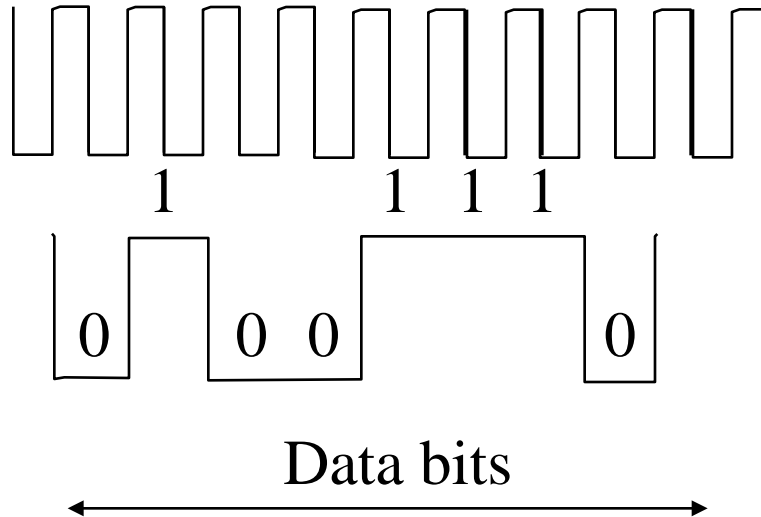
Introduction: Parallel Communication

- Timing circuits: counters and clocks
 - Real-time applications require independent clocks that are not affected by processor operations
- Parallel I/O port, parallel interface adapter



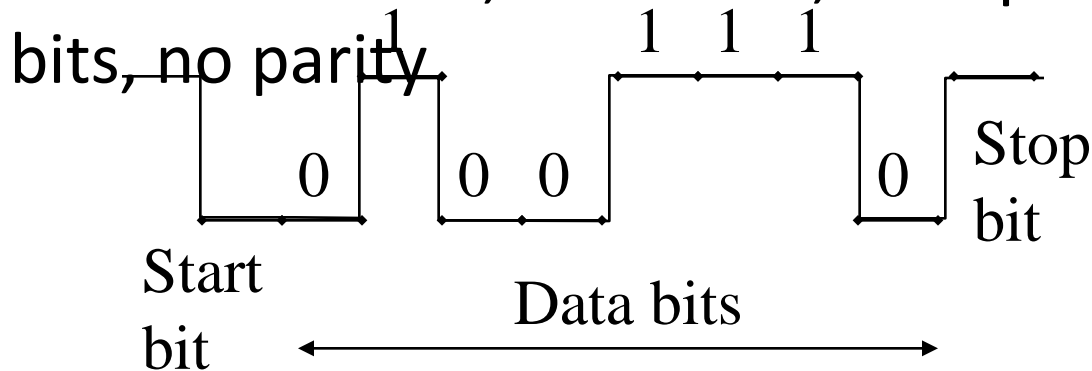
Introduction: Serial Communication

- Serial I/O port: transmission and reception one bit at a time
- Synchronous serial communication: separate clock signal



Introduction: Serial Communication

- Asynchronous serial communication
 - Start/stop/parity bits, baud rate (bits per sec.)
 - Universal Asynchronous Receiver Transmitter (UART)
 - Example of asynchronous serial communication, 1 start bit, 1 stop bit, 8 data bits, no parity



Introduction: RS-232



- Voltage level, DB-25, DB-9 connectors, ~20 kbaud (k-bits/sec), 50 ft. Physical-electrical-functional standards.
- As few as 3 pins used.
- Null modem or crossover cable: connection between computers instead of computer to device.

Introduction: Plug-in-slots



- Slots: electrical connections to CPU and other parts
 - Diskette drive, serial port, memory expansion, data acquisition and control, sound card.
 - Configuration: interrupt request level (IRQ), I/O port address, direct memory access (DMA) channels

Introduction: Bus



- Bus:
 - Industrial Standard Architecture (ISA),
Extended ISA (EISA)
 - The “plug-and-play” concept
 - Peripheral Component Interconnect (PCI) bus:
 - PCI chip between slots and processor, uses registers to store configuration info
 - high throughput tasks
 - No need for jumpers or dip switches and no conflicts

Introduction: Bus



- Personal Computer Memory Card International Association (PCMCIA)
 - Memory and modems for portables.
 - More devices (Ethernet, SCSI interface, CD-burners, data acquisition, etc)
 - Fast access (but recent USB standard offers a convenient alternative)
- Small Computer System Interface (SCSI): high speed parallel interface bus (daisy chain)

Introduction: Computer Languages



- Machine-assembly
- BASIC (high-level, interpreter-based, low storage requirements)
- C (high level, transportable, efficient)
- MATLAB (and others; C-based-kernel, arrays, very-high-level math macros $\text{inv}(A)$, $A*B$)
- Simulink: MATLAB GUI, system simulation, block diagram definitions

Introduction: Computer Languages

- MATLAB/SIMULINK: expansion via toolboxes (collection of functions written in MATLAB, (or C, Fortran, then converted to an executable .dll or .mex for older versions)
- Recent developments: ability to compile MATLAB code and create stand-alone executables
- xPC, xPC-target: real-time stand-alone applications from SIMULINK code

Introduction: Computer Languages

- xPC: Ability to perform rapid prototyping by constructing real-time code with very-high-level GUI.
 - Good for standard I/O interfacing
 - Easy-to-maintain code (SIMULINK)
 - More complicated applications may require the development of new interface drivers
 - More info: on-line or web help from mathworks

Introduction: MATLAB



- MATLAB: Initially, computations with arrays e.g., $A*b$, $A\b$, $\text{eig}(A)$, $\text{svd}(A)$. Then expanded to address all “signal and system” topics.
- Basic file structure:
 - m-files: scripts or functions, with high level interpreter commands
 - mat-files: data in binary format (see LOAD/SAVE)
 - .dll: executable code

Introduction: MATLAB



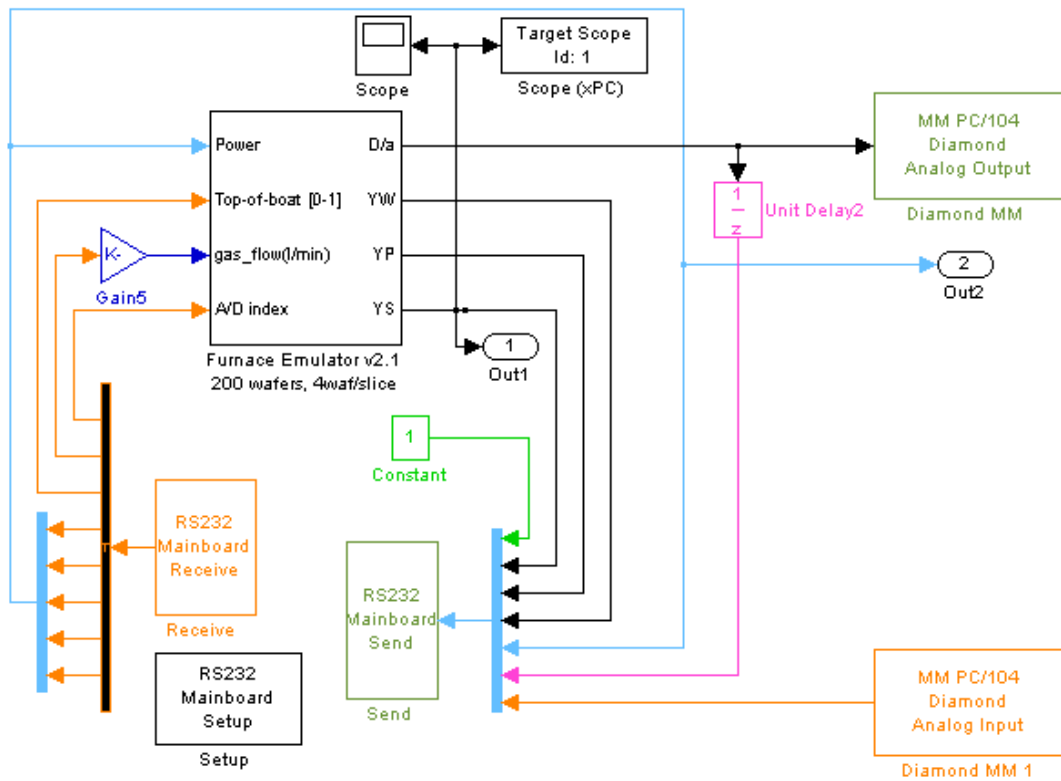
- Other commands
 - “help:” the most important command...
 - Commands for systems, control, signal processing, image processing, neural networks, ...
 - arranged in “toolboxes”, i.e. directories with m-files
 - tree structure is only important for indexing and help but not for operation
 - Matlab will only look in the defined “path” for functions and data. A useful trick is to copy a shortcut in each data directory having an empty option at “Start in”. Then, double click the shortcut to open a MATLAB session and include the current directory in the path.

Introduction: MATLAB



- SIMULINK: MATLAB GUI to define simulation systems in block-diagram form
 - mixed continuous and discrete time, but not as “easy” as it used to be...
 - .mdl files contain an ASCII description of the parameters of each block
 - s-functions: key building block of the simulator, relying on the concept of the state; fairly easy to create custom blocks but becomes complicated if real time executables are created

Introduction: MATLAB

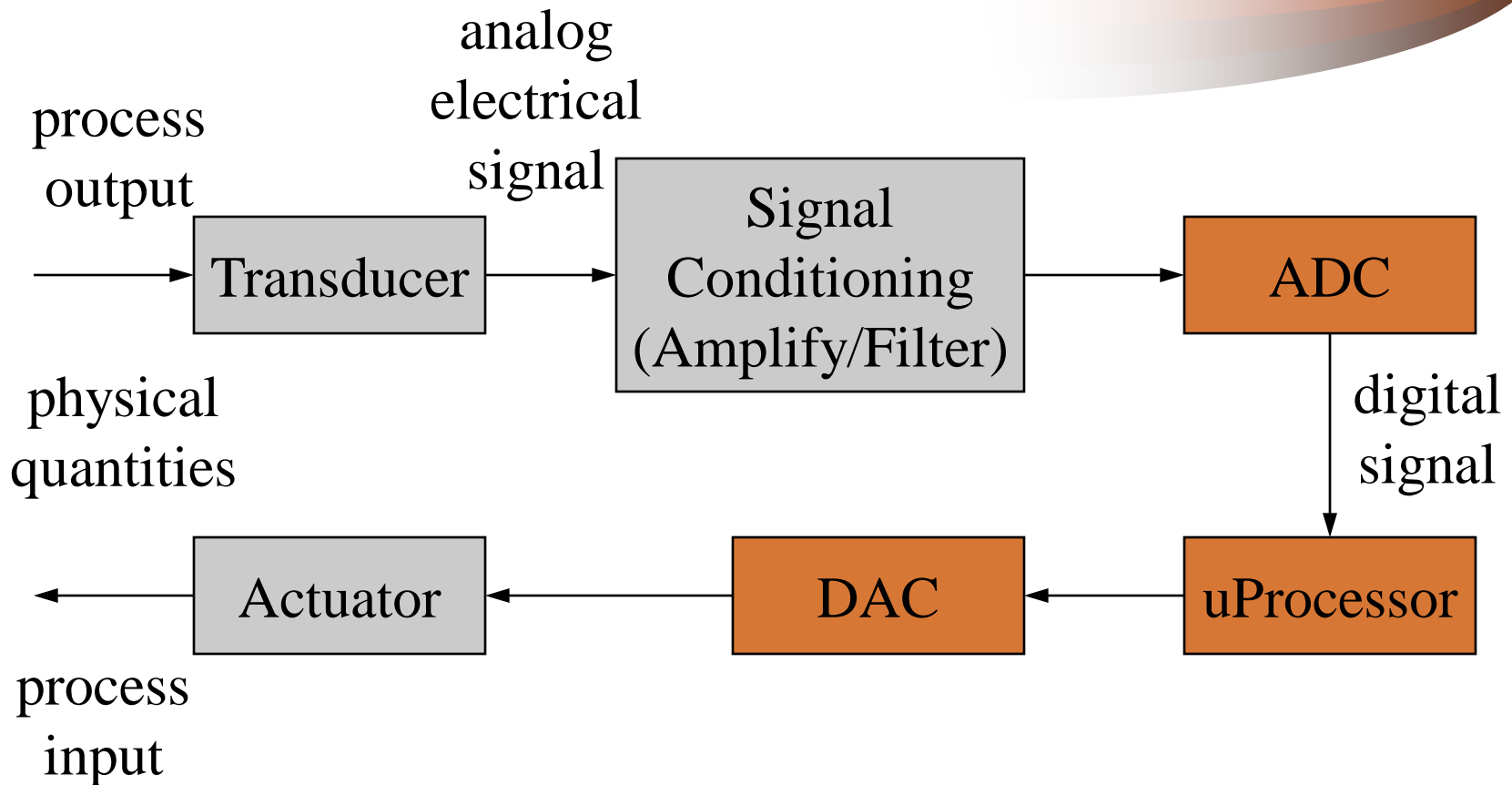


A SIMULINK example with:

- A main block (Furnace emulator),
- RS-232 I/O,
- Analog I/O, and
- Screen output

More details in
Furnace Notes.doc

Typical Configuration of a data acquisition and control system



Computer Interfacing for Data Acquisition and Control



- Data acquisition: discretization in time and quantization in state-space
- Sampling theorem, Nyquist frequency.
 - No-aliasing condition: $T_{\text{sample}} = 1/(2 f_{\text{max}})$
 - Practical selection: $T_{\text{sample}} = 1/(20f_{\text{max}})$
 - Use of anti-aliasing filters (Review!)
- Quantization resolution = full scale/ 2^n

Digital Signals



- PLC (Programmable Logic Controllers): well suited for Boolean Algebra implementations
 - E.g., Alarm when
 - low level and high pressure
 - high level and high temperature
 - high level and low temperature and high pressure
 - Analog implementation of a two-level signal with hysteresis: op-amp with positive feedback

Digital Components



- TTL, CMOS
 - Digital logic circuits will not drive actuators directly
- Electromechanical or solid-state relays
 - Switch high currents and voltages
 - Considerations: wear, corrosion, arcing, robustness, speed, noise immunity
- Encoders, counters, latches, tri-state buffers

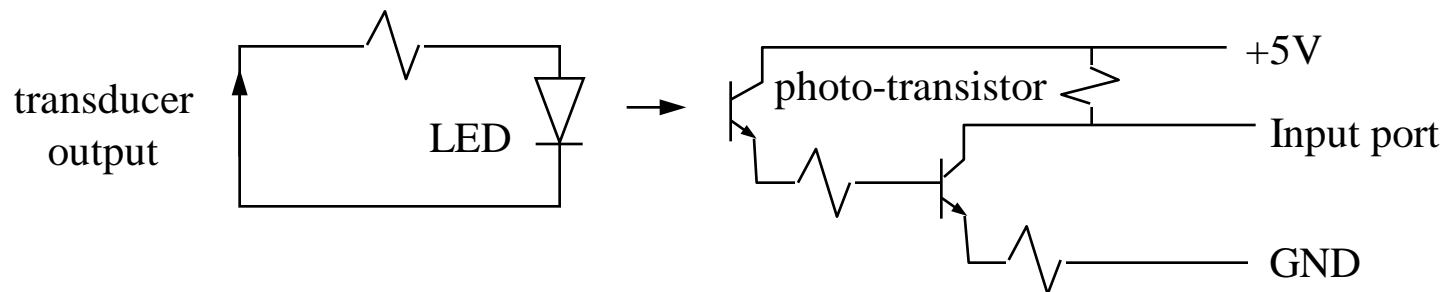
Analog Circuitry



- The 4-20mA standard: current signal information ranging between 4 and 20mA.
 - 4mA minimum to check integrity, 20mA maximum to indicate malfunctions
 - can drive various instrumentation devices with standardized input
 - many actuators follow the same standard and work with 4-20mA inputs
 - 3-15psi (20-100kPa) pneumatic loop standard

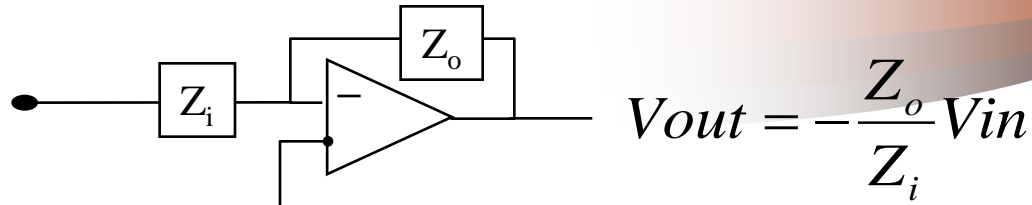
Analog Circuitry

- Signal buffering with op-amps
 - voltage following to minimize loading in the sensor and electrically isolate the sensor from the circuit
- Offset correction, filtering of unwanted frequencies (typically with low-pass filters)
- Isolation: opto-couplers, magnetic coupling



Analog Circuitry

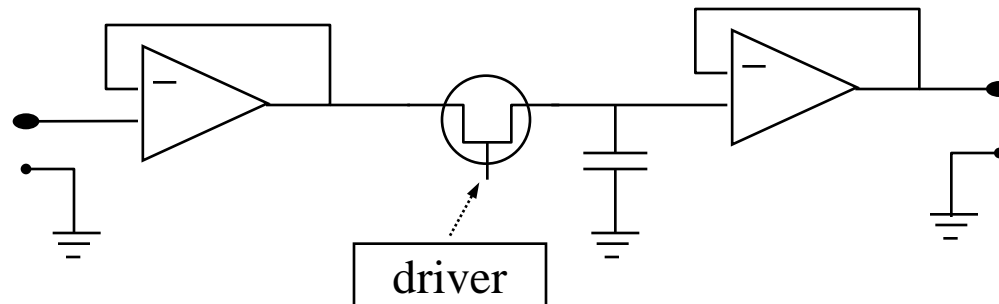
- Op-amps:



- Active filters, low-pass, high pass, notch, etc.
- Voltage followers (high input impedance, low output impedance)
- Summation, difference, current-to-voltage conversion, voltage-to-current conversion
- Nonlinear function inversion (when $Z_o = \text{diode}$ (exponential $i = e^{aV_o}$) => logarithmic amplifier

Analog Circuitry

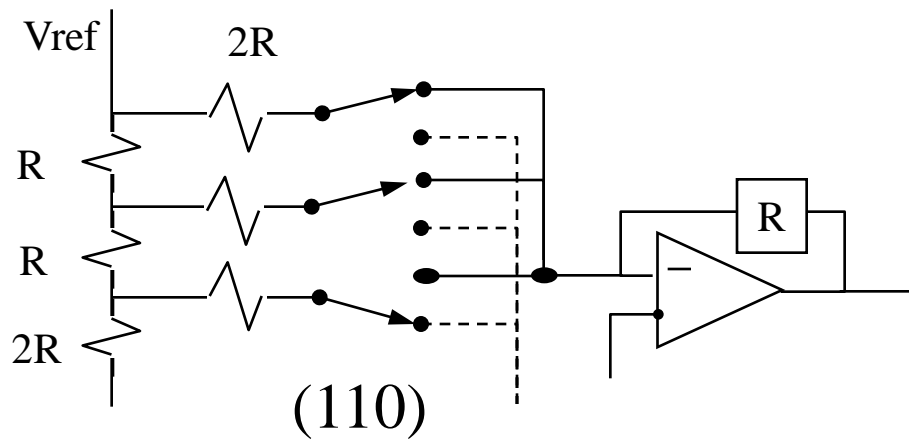
- Analog Switches (JFET, MOSFET).
 - In Multiplexers and Sample-and-Hold circuits
 - S&H example:
 - computer controlled switch (digital out)
 - hi-quality capacitor maintains “constant” voltage during conversion time



DAC-ADC

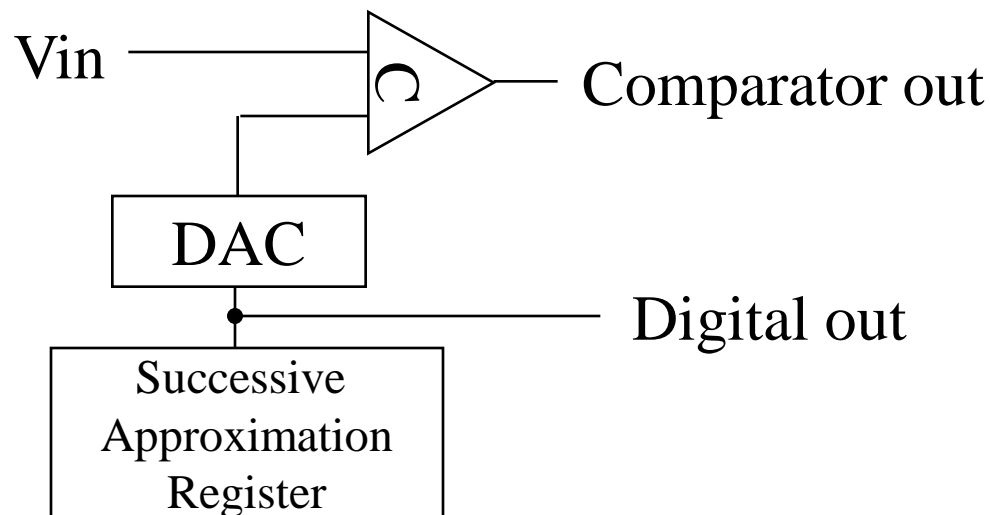
- DAC

- “Binary ladder” networks (requires large resistances)
- “R-2R ladder” network



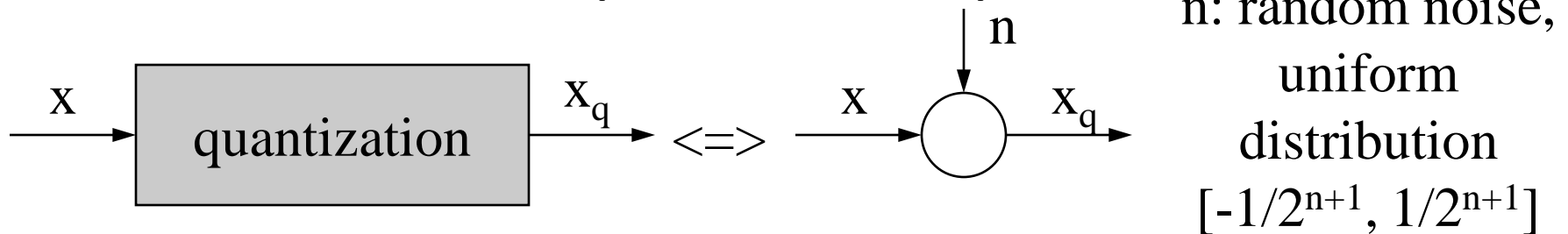
DAC-ADC

- ADC
 - Counter or ramp (slow, 2^n cycles)
 - Dual slope (noise averaging, slow)
 - Successive Approximation (fast, n cycles)



Quantization

- A special type of error: uncertainty reduction but with reduced accuracy
- 12-bit A/D, 0-5V $\Rightarrow 5/2^{12} = 1.2\text{mV}$ resolution
- Model of the quantization process



- Signal conditioning: Scaling to full range

Quantization

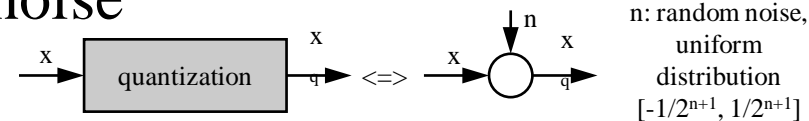


- Need for scaling:
 - Temperature range 0-2000°C. Thermocouple output 0-30mV (assumed linear). 12bit A/D, 0-5V. Resolution: 1.2mV (from before) ~
 $(2000/30\text{m}) * 1.2\text{m} = 80 \text{ }^\circ\text{C} \Rightarrow \text{measurement} = \text{value} \pm 40^\circ\text{C}!$
 - Amplify TC measurement by $5/0.03 = 166.67$.
Resolution: $(2000/5) * 1.2\text{m} = 0.48 \text{ }^\circ\text{C}$
(reasonable)

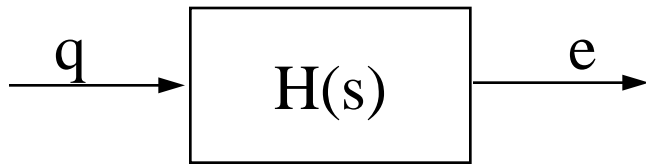
Quantization II

- Quantization issues in Filtering and Control

- Finite precision introduces errors in the computations as well as in the filter implementation.
- Fixed-point arithmetic: bounded noise
- 3 classes of errors:

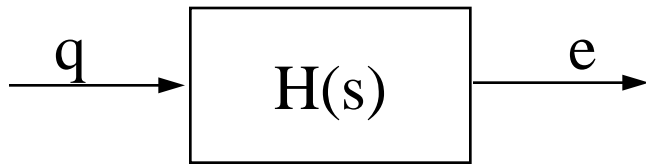


- 1. A/D conversion: Type 1 errors due to signal quantization. Typical error is $1/2$ LSB
- Multiplication: Type 2 errors due to signal quantization and truncation. Loss of several LSBs
- Coefficients: Type 3 errors due to finite wordlength in filter implementation. Can cause filter instability. More important in FeedForward control.



Quantization II

- Type 1 and 2 quantization errors
 - Modeled as independent random noise with uniform distribution.
 - Error analysis: Compute the overall transfer function $H(s)$ from the quantization error(s) “ q ” to the output of interest “ e ” and use an appropriate metric to quantify the effect of q on e
 1. Maximum error bound (very conservative)
 2. RMS error bound (usually conservative)
 3. Variance (good estimate, most appropriate for this case)
- Note: The conservatism of the estimate does not mean that the metric is not important, just that the analysis is not tight.



Quantization II

- Error bounds:

Max.Amplitude: $\|e\|_{\infty} \leq \|H\|_{i\infty} \|q\|_{\infty}$

where: $\|H\|_{i\infty} = \int |h(t)| dt$, $h(t) = L^{-1}\{H(s)\}$

(MATLAB: `sum(abs(impz(H)))*DT`)

RMS: $\|e\|_{RMS} \leq \|H\|_{i2} \|q\|_{RMS}$

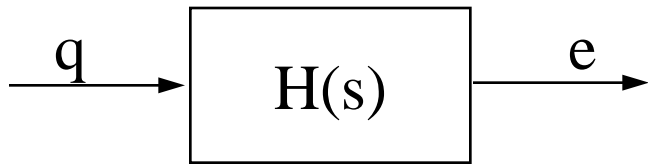
where: $\|H\|_{i2} = \max_w |H(jw)|$ (for stable H)

(MATLAB: `norm(H,inf)`)

Variance: $\text{var}(e) \leq \|H\|_2^2 \text{var}(q)$

where: $\|H\|_2^2 = \frac{1}{2\pi} \int \text{trace}(H^*(jw)H(jw)) dw$

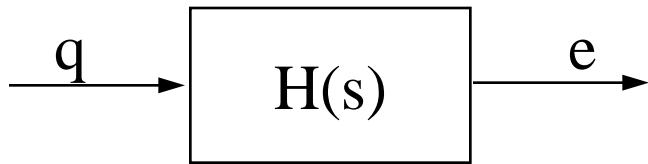
(MATLAB: `norm(H,2)`)



Quantization II

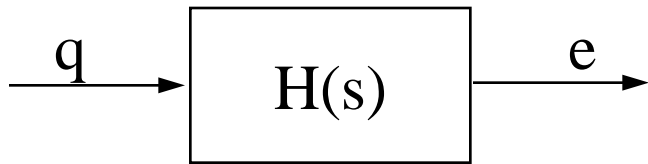
- Example:

- Consider the plant $P(s)=1/s$, with the controller $C(s)=(s+1)/s$. Analyze the effect of a 10-bit input quantization on the output.
- Discretization interval $0.01s$, ZOH
- $H = P/(1+PC) = s/(s^2+s+1)$
- $H_d = 0.01(z-1)/(z^2-1.99z+0.9901)$
- **CT:** `t=[0:.001:50]'`; `h=impulse(H,t)`; `plot(t,h)`; `Hii=sum(abs(h))*0.001`
- `Hii=1.306`, `Hi2=norm(H,inf)=1`, `H22=norm(H,2)^2=0.5`
- **DT:** `k=[0:10000]'`; `h=impulse(Hd,k*.01)`; `plot(k,h)`; `Hii=sum(abs(h))`
- `Hii=1.3181`, `Hi2=norm(H,inf)=1.0044`, `H22=norm(H,2)^2=0.0051`



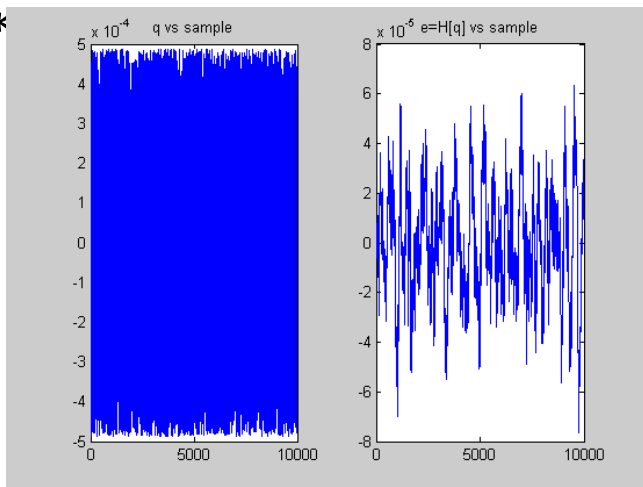
Quantization II

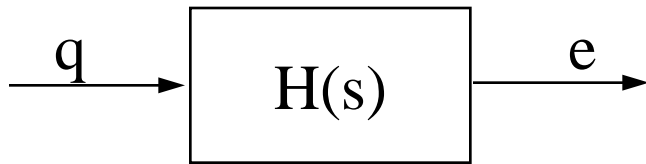
- Example (cont): Compute bound estimates
 - $q_{\max} = 1/2^{11}$, variance (uniform density) = $q_{\max}^2/3 = 7.947e-8$,
RMS $\sim \text{sqrt}(\text{var}) = 2.819e-4$
- $\max(|e|) < |H_{11}| q_{\max} = 6.4359e-004$
- $\text{RMS}(e) < |H_{12}| \text{RMS}(q) = 2.8313e-004$
- $\text{var}(e) < |H_{22}| \text{var}(q) = 4.0337e-010$
- The variance estimate appears to be much better than the RMS: $\text{sqrt}\{\text{var}\} = 2.0084e-005 \ll 2.8313e-004$



Quantization II

- Example (cont): Evaluate the estimates by simulation
- `qm=1/2^11 ;q=(rand(10000,1)-0.5)*2*qm;k=[0:10000-1];subplot(121),plot(k,q), title('q vs sample')`
- `Hd=fbk(c2d(P,.01),c2d(C,.01)),e=lsim(Hd,q);subplot(122),plot(k,e),title('e=H[q] vs sample')`
- `[max(abs(e)),sum(abs(h))*max(abs(q))]` = 6.2659e-005 6.4352e-004
- `[rms(e),norm(H,inf)*rms(q)]` = 1.9416e-005 2.7953e-004
- `[var(e),norm(H,2)^2*`





Quantization II

• Comments:

- The max abs estimate is conservative by an order of magnitude.
- The var estimate is much better than the RMS.
- However, from the theory we know that the RMS bound is tight. The apparent discrepancy is due to the fact that var is defined for stochastic signals and RMS^2 is just its estimate from one realization. The variance estimate is good for stochastic inputs only and it is not an upper bound for deterministic signals as the next computation shows:
 - $z=\sin(.01*k); y=\text{lsim}(H,z);$
 - $[\text{rms}(y),\text{norm}(H,\text{inf})*\text{rms}(z)]=7.0490\text{e-}001 \ 7.1171\text{e-}001$
 - $[\text{var}(y),\text{norm}(H,2)^2*\text{var}(z)]=4.9686\text{e-}001 \ 2.5490\text{e-}003$
 - Notice that $\text{norm}(H,2)^2*\text{var}(z)$ is NOT a bound on $\text{var}(y)$ any more!
 - But the bound $\text{norm}(H,\text{inf}) * \text{rms}(z)$ on $\text{rms}(y)$ is now tight.

Quantization II

- Quantization issues in Filtering and Control
 - Due to the sensitivity of roots of polynomials to perturbations, the quantization of the filter coefficients can result in a different, possibly unstable filter
 - Different filter realizations can be more or less susceptible to quantization problems (parallel or cascades of 1st or 2nd order are preferred over direct forms)
 - Problems become more pronounced as the sampling rate increases (the discrete poles accumulate around 1 and there is loss of resolution)

Quantization II

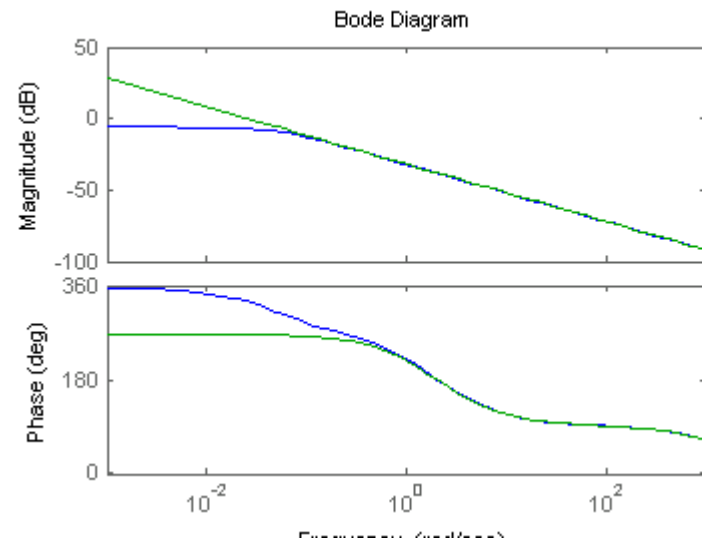
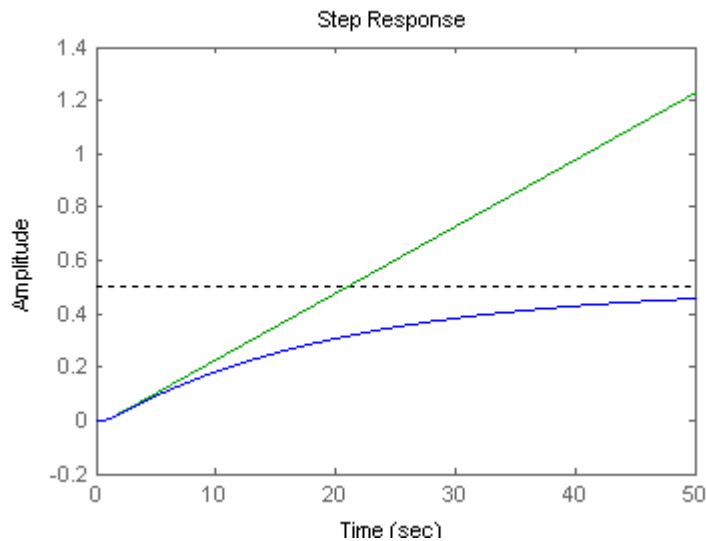


- Example

- Start with the heated-water-tube transfer function
- $P = \text{tf}([-0.5 \ 1], [0.5 \ 1]) * \text{tf}(1, [40 \ 2])$
- Discretize: $PD = \text{c2d}(P, .001)$
- Enter the same transfer function with 4 significant digits:
 $PD2 = \text{tf}([-2.495\text{e-}5 \ 2.5\text{e-}5], [1 \ -1.998 \ .998])$
- The first is stable with poles $9.9995\text{e-}00, 9.9800\text{e-}001$
- The second is unstable with poles $1.0000\text{e+}000, 9.9800\text{e-}001$

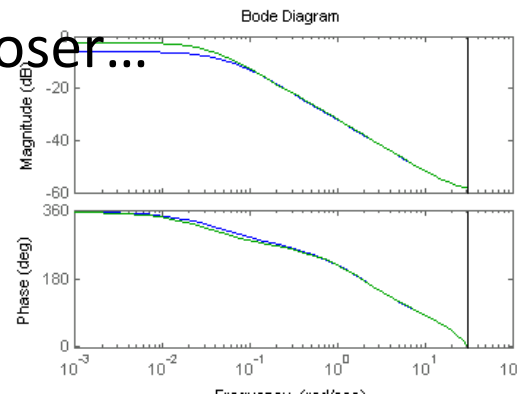
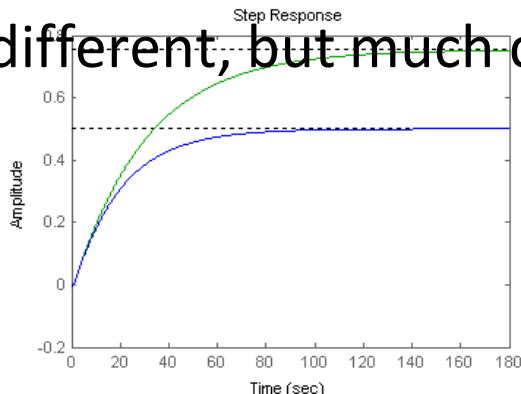
Quantization II

- The difference is apparent in terms of step and frequency response



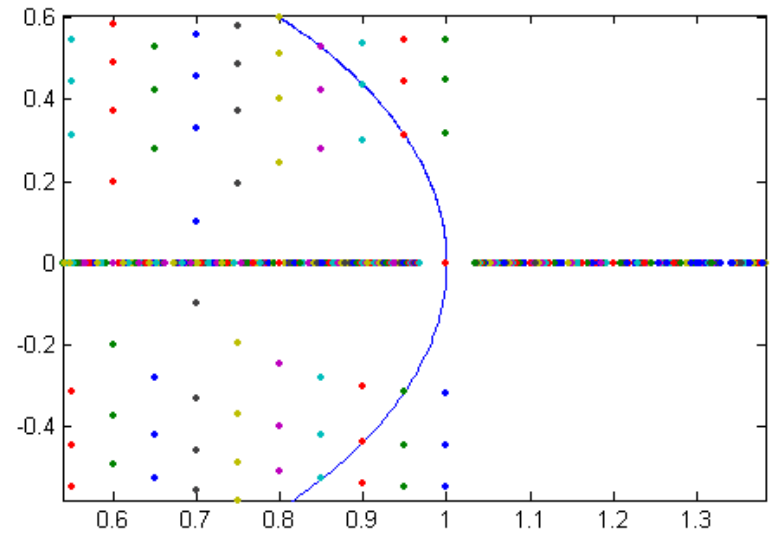
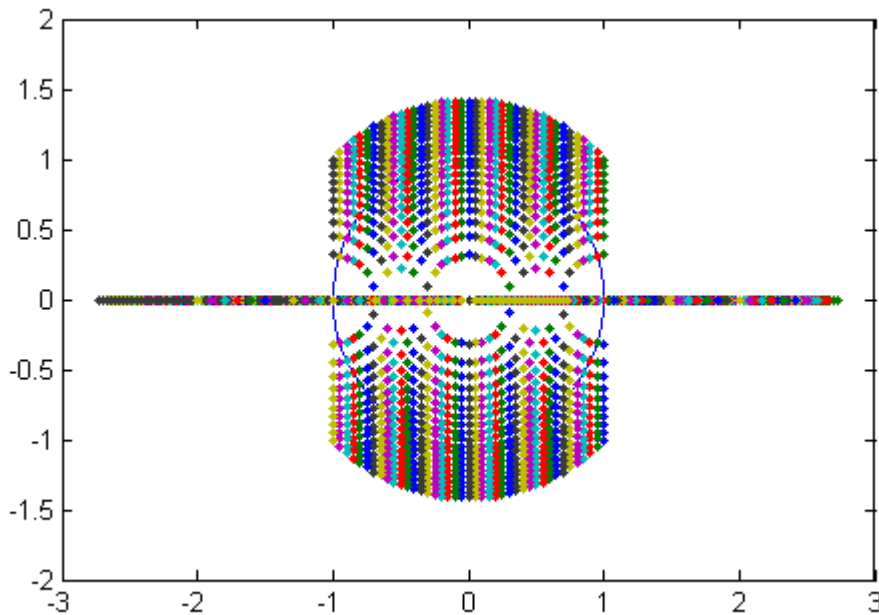
Quantization II

- Repeat for sampling time 0.1:
- Discretize: $PD=c2d(P,.1)$
- Enter the same transfer function with 4 significant digits:
 $PD2=tf([-0.002026 \ 0.002478],[1 \ -1.814 \ 0.8146],.1)$
- The first is stable with poles $9.9501e-001 \ 8.1873e-001$
- The second is stable with poles $9.9672e-001 \ 8.1728e-001$
- Still different, but much closer...



Quantization II

- Some insight
 - roots of 2nd order polynomial whose coefficients, are quantized to 0.1



Cables



- Flat cables: 1-10V, 100mA
- Twisted pair, shielded or unshielded
- Coaxial (less interference but not too popular)
- Digital connections, cheaper for low data rates
- Buffering (amplifying) and latching, for signals on a bus

Data acquisition and control with standard add-on cards



- Multifunctional cards: A/D, D/A, digital I/O, counter/timer operations
 - 4-16 multiplexed A/D, 1-2 D/A, (max rate quoted for all channels combined)
 - programming commands (in C or high-level)
- Industrial signal conditioners
 - thermocouple linearization and cold junction compensation, filtering and amplification, strain gauge linearization, etc.

Data acquisition and control with standard add-on cards



- Signal Conditioning Extensions for Instrumentation (SCXI): high performance system for use with PCI
- Remote I/O modules. Standard RS-232, RS-485 interfaces for 15-bit measurement resolution
- IEEE-488 GPIB (general purpose interface bus)
 - rigidly defined, 1Mbyte/s transfer rates, multiple (15) devices to a single network

Data acquisition and control with standard add-on cards



- IEEE-488 GPIB hardware specs
 - total cable length 20m, individual device cable 2m
 - 24 lines in the cable, clearly defined; 8 data, 8 handshaking, 8 grounding and shielding
 - star, daisy chain, mixed networks
- GPIB devices
 - Talkers, listeners, controllers; interconnected via back plane.

Data acquisition and control with standard add-on cards



- Backplane Bus
 - Board on which connectors are mounted; provides data, address, control signals
- STE Bus
 - 8 bit, 20 address lines (1MB memory), 4kB addressable I/O
 - Compact cards, robust two part connector, shock and vibration resistant
 - IEEE-1000 standard

Data acquisition and control with standard add-on cards



- VME Bus
 - Motorola design for the 32 bit 68000-based system.
 - 24MHz data transfer rate
 - 32 bit address bus
- VXI Bus (VME extension for instrumentation)
 - Improvement over GPIB in communication speed, synchronization and triggering
 - Various possible system configurations including GPIB

Microcontrollers



- Microprocessors with analog and binary I/O, timers, counters, to perform real-time control functions (8, 16, 32 bit)
 - Characteristics: 4kB ROM, 128B RAM, single byte instructions, built-in counters, timers, I/O ports
 - Intel 8051, 8096, Motorola MCH68HC11, etc.
 - DSP (Digital Signal Processors): special architecture for high speed numerical tasks. Separate data bus from instruction bus.

Microcontrollers



- The Arduino family
 - Inexpensive evaluation boards (low-medium capabilities)
 - Available drivers making their programming easy (albeit with some restrictions)
 - Large development forums (software and 3rd party hardware support)

Distributed Digital Control Systems



- Increased complexity is less of an issue
- Additional functions over older analog systems (redundancy, failure detection, communication, data storage, adaptation/scheduling)
- Overall more reliable, less susceptible to computational noise, controllers are not degrading with time
- Low cost

Distributed Digital Control Systems



- Process control applications
 - Plant automation
 - Programmable logic controllers (PLC, sequencing jobs)
 - Regulatory process control: single loop PID or Distributed Control System (DCS) for large-scale applications
 - Batch processes: repetitive nature; “run-to-run” optimization schemes
 - Advanced applications (identification and control)

Distributed Digital Control Systems



- Computer networks, different topologies
 - For control over networks, the issues of reliability, and deterministic message transmission must be addressed
 - Network communications: common modular set of rules for generating and interpreting messages
 - Open System Interconnection (OSI): 7-layer architecture; Physical, Data link, Network, Transport, Session, Presentation, Application

Distributed Digital Control Systems



- OSI components
 - Repeater, at the physical layer
 - Bridge, at data link layer
 - Router, at network layer
 - Gateway, at higher levels
- Communication protocols define connectors, cables, signals, data formats, error checking, algorithms for network interfaces and nodes

Distributed Digital Control Systems



- Communication protocols
 - Simple: polling and interrupt driven
 - Token ring and Token Bus
 - Carrier sense multiple access with collision detection (CSMA/CD)
 - IEEE 802.3. Check for network activity. If idle, a node may transmit, then the network becomes busy. In case of collision, transmission is aborted and a random wait time is introduced.

Distributed Digital Control Systems



– CSMA/CD

- Simple algorithm, non-deterministic, priorities not supported, collisions a problem at high network loads, analog technology for collision detection
- Ethernet is an implementation of CSMA/CD network. 10Mb/s, coaxial cable or twisted pair. E.g., National Semiconductor 3-chip implementation: Network interface controller (protocol, information movement), Serial network interface (clock), Coaxial transceiver interface (coaxial versions)

– Token ring and Token Bus

Distributed Digital Control Systems



- Several DCS platforms from major manufacturers
 - Honeywell, Foxboro, Fisher and Porter, Westinghouse, EMC control, Reliance Electric, Beckman Instruments
- Recently, PC or workstation based systems, supervising local embedded controller boards

Examples of Computer Control



- Industrial processes versus laboratory experiments
- Several aspects:
 - Process description and modeling
 - Sensors and actuators
 - Controller design (algorithm and structure)
 - Discretization and implementation
 - Auxiliary functionality

Examples of Computer Control



- Liquid level system
 - Tank - valve - pump in different configurations
 - Differential pressure transducer (translating to level). Other options: floaters, resistivity measurements.
 - Valve as a final control element (with or without a pump). Electric valve, pneumatic valve (common), electric actuation via I/P current-to-pressure converter

Analysis of the Liquid Level Control Experiment

- One example: control the level by manipulating the inlet stream or the outlet.

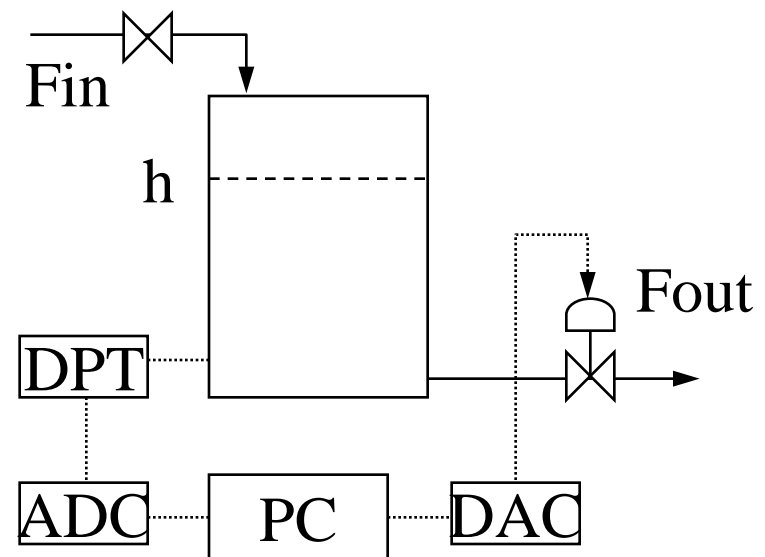
- F_{in} , F_{out} : flowrates in and out. h : level

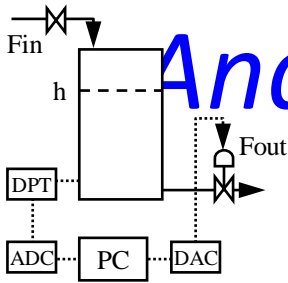
- Bernoulli:

$$P + \frac{1}{2} \rho v^2 + \rho g h = const.$$

- P : pressure, ρ : density,

- g : grav. accel., v : velocity





Analysis of the Liquid Level Control Experiment

$$A_i \dot{h}_i = F_{in} - F_{out}$$

– inlet conditions

$$A_i v_i = A_o v_o$$

– incompressible flow

$$P_i + \frac{1}{2} \rho v_i^2 + \rho g h_i = P_o + \frac{1}{2} \rho v_o^2 + \rho g h_o$$

– Bernoulli

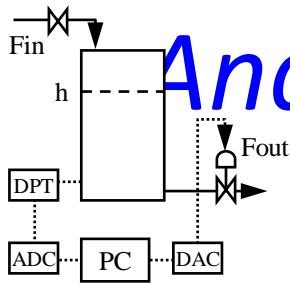
$$P_i = P_o, h_o = 0, A_i \gg A_o \Rightarrow v_i \ll v_o \Rightarrow 2gh_i \cong v_o^2$$

$$\Rightarrow A_i \dot{h}_i = F_{in} - A_o v_o = F_{in} - A_o \sqrt{2gh_i}$$

– simplify

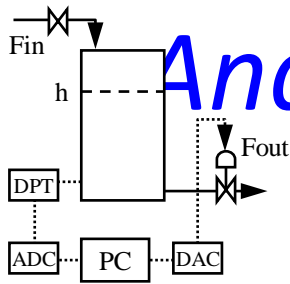
$$\Rightarrow \dot{h}_i = \frac{F_{in}}{A_i} - \frac{A_o}{A_i} \sqrt{2gh_i}$$

- A = cross section area, inlet-outlet
- “Ideal” flow



Analysis of the Liquid Level Control Experiment

- ODE for h , nonlinear: slower than linear response for large levels h ; faster for small h .
 - Tank drains in finite time
 - Addition of a pump: reduced sensitivity of outflow to liquid level in the tank
- Next, the manipulated variable: We open or close the valve, i.e., we effectively modify the outlet cross section area.

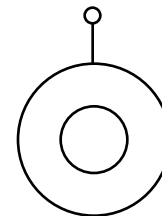
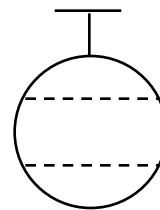


Analysis of the Liquid Level Control Experiment

• Valves

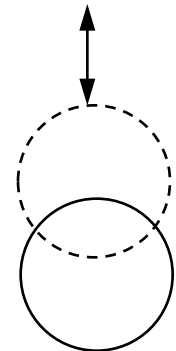
- Many types with different characteristics (pressure drop, open/close speed, size, linearity, sealing).
- Ball (common, e.g., manual/auto sprinkler valves at the store)

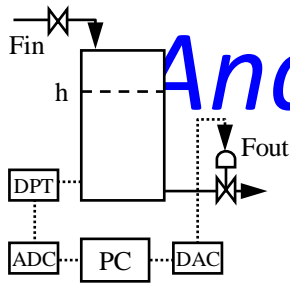
Ball, side and front view
(spherical housing not shown)



- Gate (sliding in and out to restrict flow)
 - easier to compute cross section area

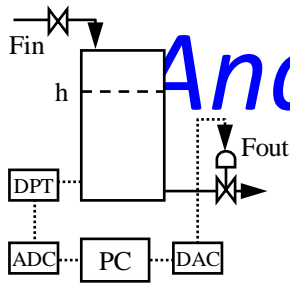
Disc-shaped Gate, front view





Analysis of the Liquid Level Control Experiment

- Let us select a gate valve with a motorized screw as an opening/closing mechanism.
- We manipulate the current to the motor or, in a high friction simplification, the motor speed.
 - Suppose that at max speed, it takes 2 sec from full-open to full-close
- Other options: Manipulate the set-point of a valve controller, for a %-open value; pneumatic valves with a I/P converter.



Analysis of the Liquid Level Control Experiment

- Compute cross section area as a function of %-open (distance between gate center and pipe center)

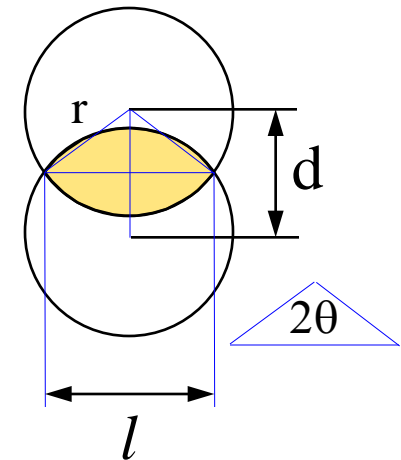
– shaded area = $2 \times [\text{sector} - \text{triangle area}]$

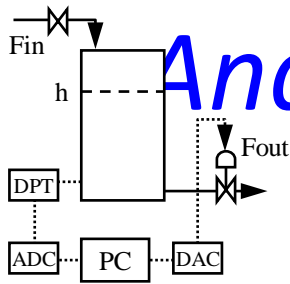
– $\theta = \cos^{-1}(d/2r)$, $SECTOR.AREA = r^2 \cos^{-1}(d/2r)$

$TRIANGLE.AREA = ld / 4$, $l = \sqrt{4r^2 - d^2}$

$\Rightarrow \dots \Rightarrow A_o = 2r^2 [\cos^{-1}(D) - D\sqrt{1-D^2}]$, $D = d/2r$

– Relation to control input: $\dot{d} = u$

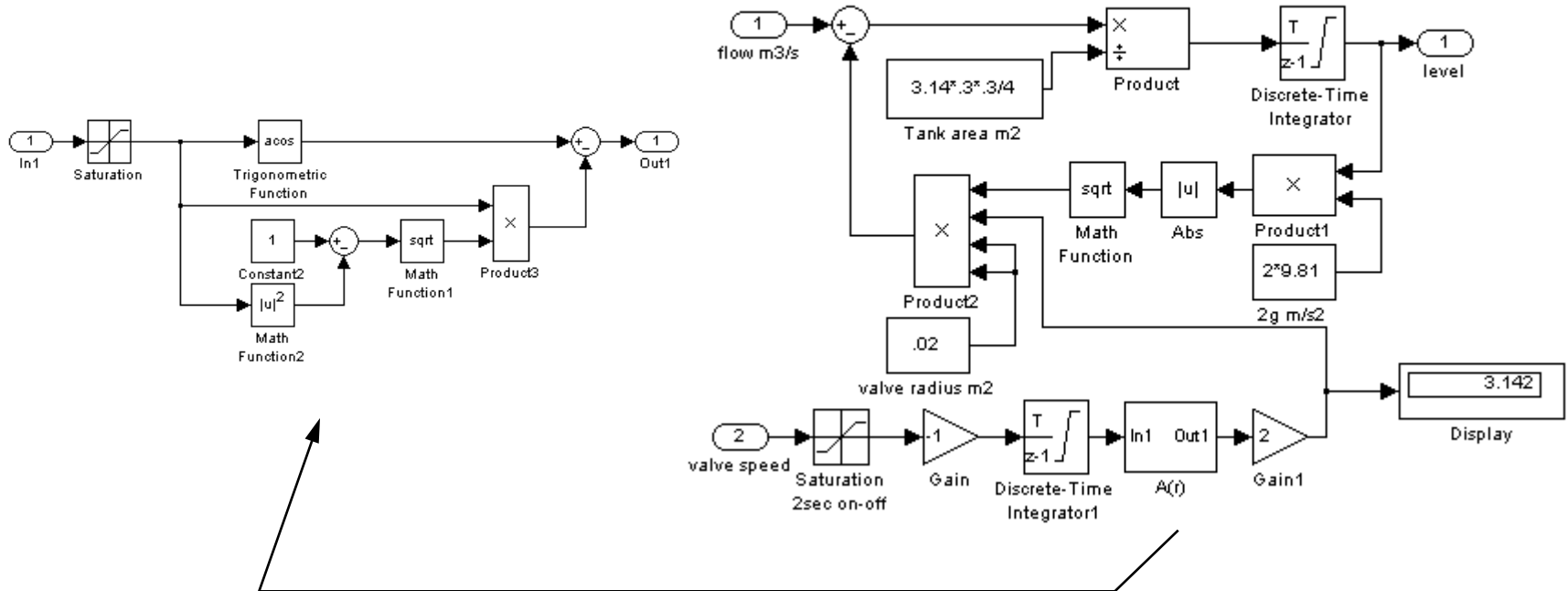


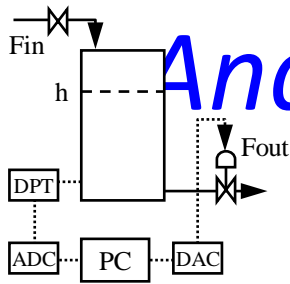


Analysis of the Liquid Level Control Experiment

- Simulink Implementation

4cm pipe diameter
 30cm tank diameter
 2sec full-on-full-off gate valve
 no friction no losses

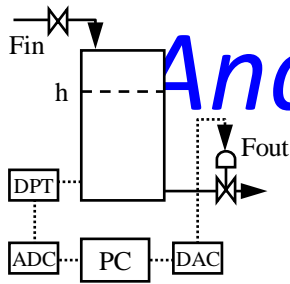




Analysis of the Liquid Level Control Experiment

- Simulink Implementation

- Test the analytical no-inlet discharge time. $\dot{h} = \alpha\sqrt{h}$
- Test analytical steady-state results for Fin constant.
- Discretization: Estimate natural time constant and controlled (closed loop) time constant; sample an order of magnitude faster; check responses visually.
- Use saturation nonlinear blocks to observe physical limitations



Analysis of the Liquid Level Control Experiment

- Simulink Implementation

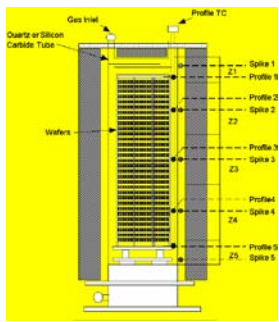
- Linearization (for analysis and controller design)

- Derive variations around a steady state, analytically or using linmod (self study)
- Parameters: 4cm pipe diam., 30cm tank diam.
- Linearization equations (at a nominal steady state where $h, D = \text{const.}$, $D \sim 0.5$, $\delta u = \text{normalized in } 0-1$)

$$\delta \dot{h}_i = - \left. \frac{A_o(D)g}{A_i \sqrt{2gh_i}} \right|_{\text{nom.ss}} \delta h_i - \left. \frac{\sqrt{2gh_i}}{A_i} \right|_{\text{nom.ss}} \left. \frac{\partial A_o(D)}{\partial D} \right|_{\text{nom.ss}} \delta D$$

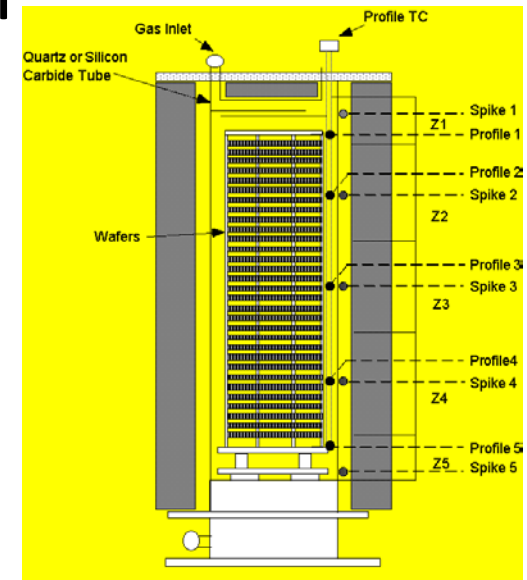
$$\delta \dot{D} = \delta u$$

Diffusion Furnace Temperature Control

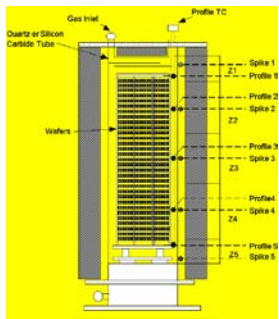


- Multivariable system, approximating distributed sensing and actuation

- Measure temperatures at different points inside the tube (profile) and outside of the tube, near the heating element (spike)
- Apply heating power through SCR actuating modules roughly in the same zones
- Accuracy is essential



Diffusion Furnace Temperature Control

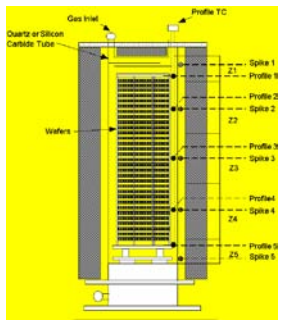


- Modeling:
 - Basic heat balance equation

$$\begin{aligned} mc_p \dot{T} &= H_{in} - H_{out} \\ &= q - hA(T - T_{ambient}) - \sigma FA(T^4 - T_{amb}^4) \end{aligned}$$

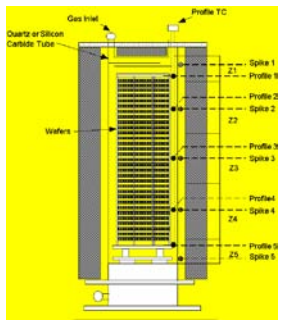
- m = mass, c_p = specific heat, T = absolute Temperature, h = heat transfer coefficient (convection), A = surface area, σ = Boltzmann constant (radiation), F = view factor, q = externally supplied heat
- Apply to differential volumes and obtain a PDE model
(details in [EEE480 model notes](#) and [EEE482 Furnace notes](#))

Diffusion Furnace Temperature Control



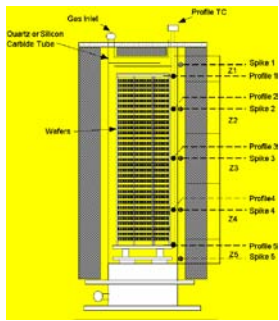
- Sensors: Thermocouples for high temperatures (some operations above 1000deg.C). Pyrometry is another option for single wafer reactors.
 - Issues: Cold-junction compensation, amplification, and table look-up linearization. RF interference may appear from SCR application of electrical power
- Actuators: SCR modules
 - Issues: resolution - switching transient trade-off

Diffusion Furnace Temperature Control



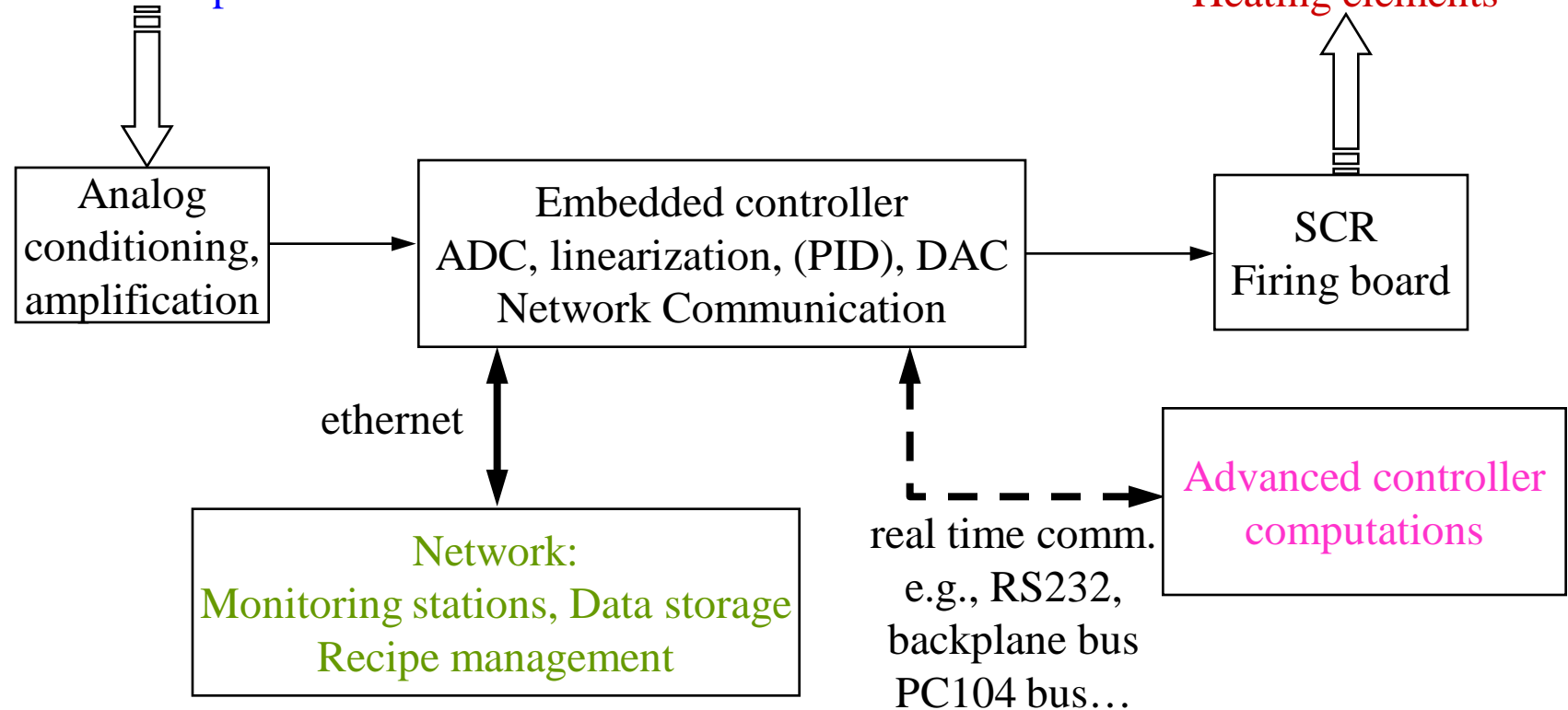
- Need for elaborate and precise controllers
 - Newer furnaces have more (5) heating zones for more resolution and improved uniformity (temperature coupling is higher than in the older 3-zone furnaces)
 - Due to radiation nonlinearity, different controllers may be necessary to cover a big temperature range
 - Nonlinearity and coupling are more pronounced in single-wafer rapid thermal processors (RTP), using arrays of heating lamps

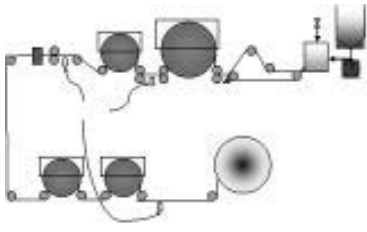
Diffusion Furnace Temperature Control



- Controller communications

Thermocouples





Control of Paper Machines

- Process description

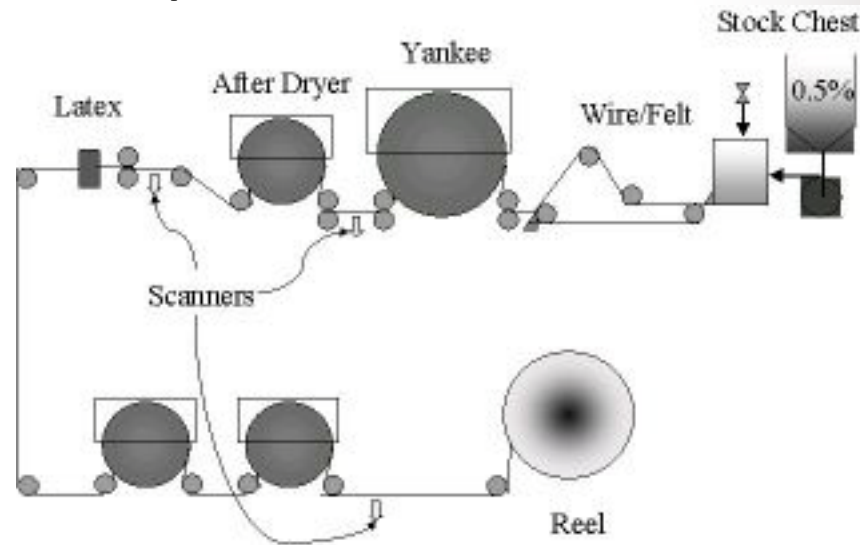
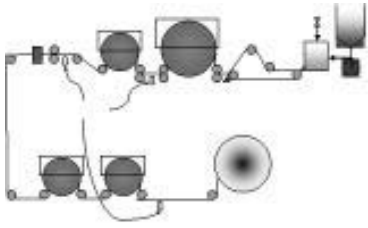


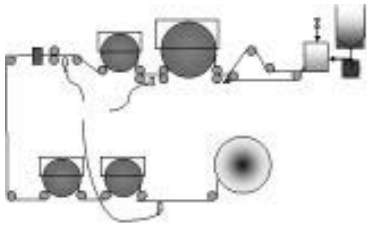
Figure 1. Paper Machine Schematic

- K. Tsakalis, S. Dash, A. Green, and W. MacArthur, "Loop-Shaping Controller Design From Input-Output Data: Application to a Paper Machine Simulator," IEEE TRANSACTIONS ON CONTROL SYSTEMS TECHNOLOGY, VOL. 10, NO. 1, 127-136, JANUARY 2002



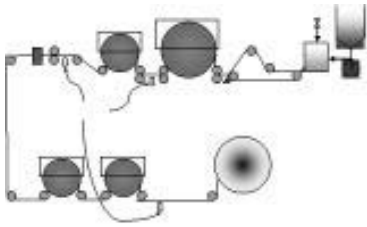
Control of Paper Machines

- **Control Inputs (manipulated variables)**
 - stock flow (solids), dryer temperatures (as set points to local PID loops), machine speed (as set point to drum motors)
- **Process Outputs (controlled variables)**
 - paper dry weight (~solids), Moisture content (at different points), machine speed (actual)
- **Disturbances**
 - Operators can change set-points in other loops to maintain the overall product quality. Feed consistency is a major disturbance, especially after paper breaks (re-circulation).



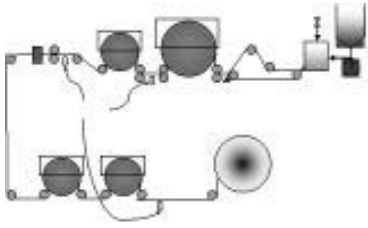
Control of Paper Machines

- Challenges in Paper Machine control
 - Consistency control (in the direction of production)
 - Cross-directional control (across the paper; distributed control, not discussed here)
 - Interacting variables, wide range of process responses. Standard decoupled single-loop control not very effective
 - E.g., Stock/Weight has long dead-time, short settling time, Steam/Moisture has short dead-time and long time constant, Machine Speed has minimal dead-time and fast dynamics. These features can have an adverse effect on both the identification and the robust control of a paper machine.



Control of Paper Machines

- Some ballpark numbers:
 - Total length of paper line ~500–1000m, speed 10–30 m/s (20–60 mi/h), dryer drums 2–3 m diam.
 - Sensors scan moisture and dry weight across the width of the paper. Scanning interval can be as large as 35 s.
 - Steam/moisture dynamics
 - ~temperature response of the drums (local PID control, closed-loop time constant in the order of a few minutes)
 - Short time-delays (scanners, drum-sensor distance), but larger delays for reel moisture (measured at the end of the line)
 - “Noise” from the interaction of the paper sheet with the environment



Control of Paper Machines

- Stock flow/dry weight dynamics
 - Larger delay since the actuator is located at the beginning of the line
 - Quick settling time, essentially determined by the stock mixing process
 - Any changes in the stock flow also have a significant effect on moisture, since it changes the net water content of the paper sheet
 - Changes in the drum temperatures or moisture leave the dry weight unaffected
- Machine speed
 - Can be controlled much faster than the other variables. Unaffected by steam or stock flow variations, but it has a significant effect on moisture and dry weight.

Heat Exchanger Control Example



- Multivariable system (see textbook), both feedback and feedforward control
 - Measure inlet temperatures and water outlet temperature (controlled variable)
 - Manipulate steam inflow, water inflow through pneumatic valves
 - Water flow is a controlled variable, either to be maximized or to track a setpoint
 - Other valves and instruments to enable monitoring and ensure integrity

Plastic Injection Molding Process

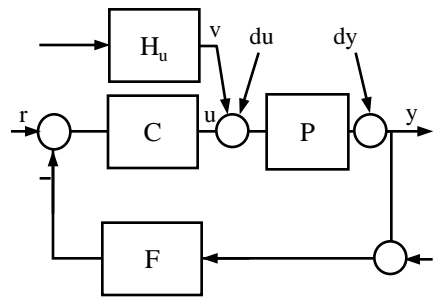


- Multivariable system, approximating distributed sensing and actuation (see textbook)
 - Measure temperatures at different points
 - Apply heating power through SCR actuating modules at the same points
 - Accuracy is important

Other Control Examples



- Aerospace applications
 - high performance fighter aircraft, helicopters, jet engines
- Electromechanical systems
 - robotic arms, pendulum, cart and pendulum
- Automotive
 - intelligent vehicle highway systems, platooning, traffic control
 - engine management, anti-lock brakes, active suspension
- Manufacturing processes, scheduling of operations

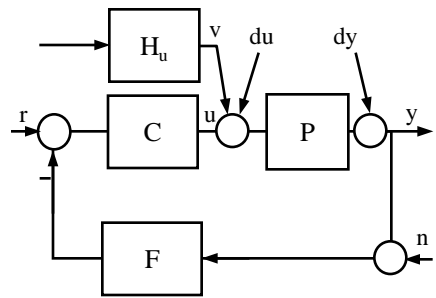


- **Controller Design Procedure:**

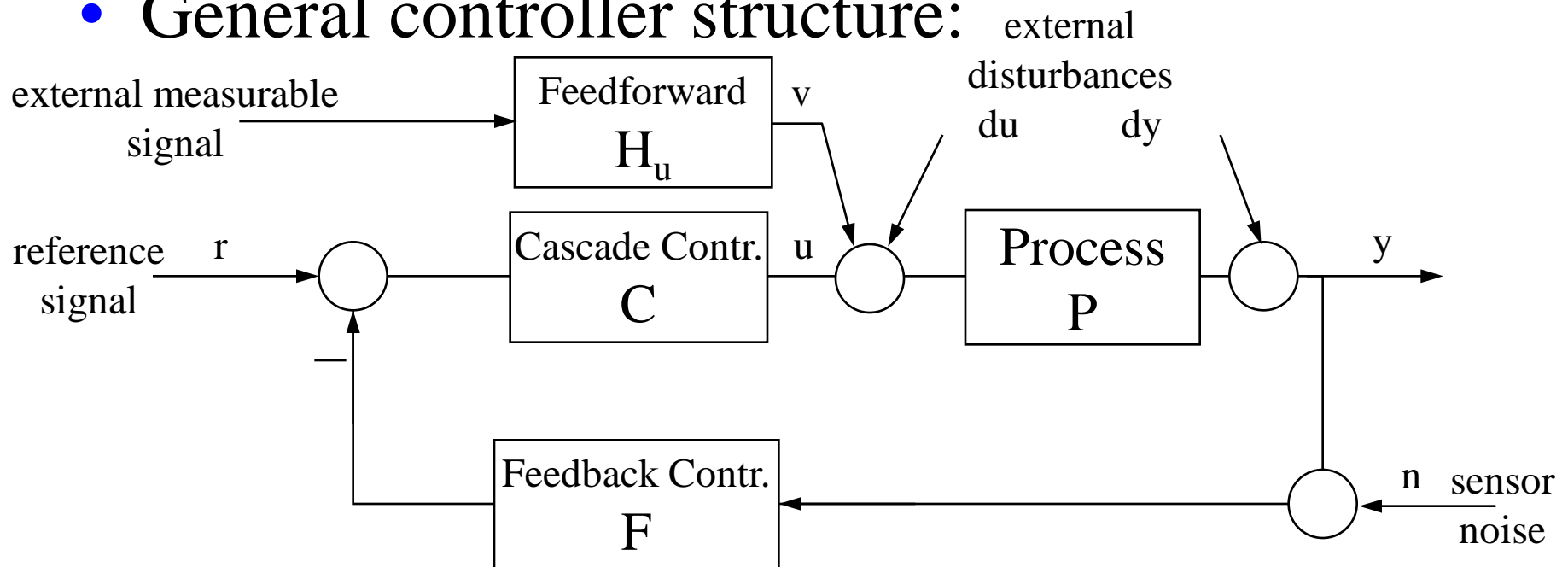
- Determine inputs and outputs
- Model or identify the system
- Define the control objectives and specifications
- **Design the controller (algorithm and parameters)**
- Discretize (if working in continuous time), quantize and implement (code + hardware)
- **Anti-windups and other nonlinear modifications: integrated (recent methods) or “post-mortem”**

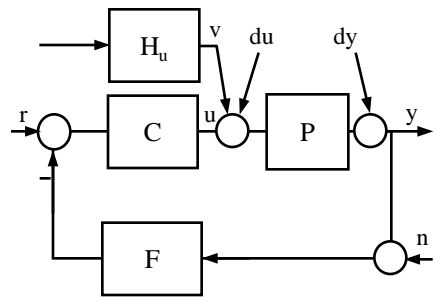
Feedback

and Feedforward Control



- On **the controller design**: computation of the transfer function(s) of the “controller”
- General controller structure:



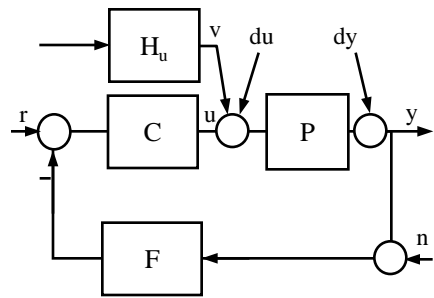


- Feedback control objective: Reduce the effect of disturbances on the output

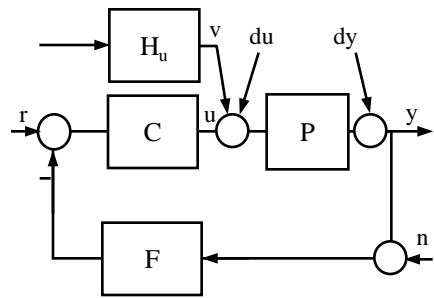
$$\begin{aligned}y &= d_y + P[u + d_u + v] \\ &= d_y + PC[r - F[y - n]] + Pd_u + Pv \\ &= Sd_y + SPCr - SPCFn + SPd_u + SPv\end{aligned}$$

where $S = (1 + PCF)^{-1}$ (Sensitivity)

- the disturbance contributions decrease when S is smaller, i.e., when CF is larger
- the noise contribution decreases when CF is smaller



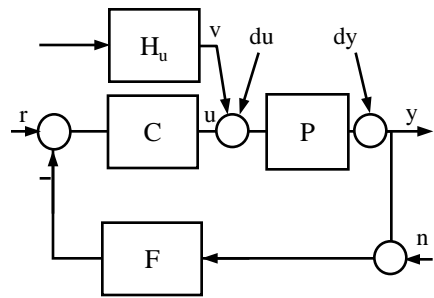
- Feedback controller design:
 - stable loop
 - PCF must produce a stable loop (crossover frequency characteristics)
 - large gain (magnitude) in the region where the sensor is reliable
 - in the same vein, respect uncertainty-imposed constraints (avoid excessive peaks/resonances in S)
 - can only attenuate disturbances where the sensor information is reliable



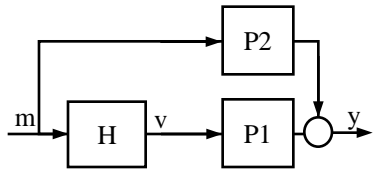
- A typical feedback controller design (math):
 - frequency domain
 - observe fundamental limitations
 - RHP poles < bandwidth < RHP zeros
 - modeling uncertainty, sensor noise => max bandwidth
 - At the gain crossover frequency

$$\omega_c : |PCF(j\omega_c)| = 1, \quad \angle PCF(j\omega_c) \approx -130 \pm 10^\circ$$

- crossover separates the frequency range of high loop gain (disturbance attenuation) and low loop gain (sensor noise attenuation). Roughly, $BW \approx 1.5\omega_c$



- Feedback controller design:
 - Software automating most of the computations
 - Tuning of PID, robust multivariable, LPV...
 - Usually, concepts are understood in terms of transfer functions and in the frequency domain but the computations are performed in the state-space relying on time-domain optimal control theory
 - Here: simple PID tuning (Ziegler-Nichols, or pidqtune)
 - Still, the selection of reasonable objectives is essential



- Feedforward control objective: cancel the effect of a measurable disturbance at the output

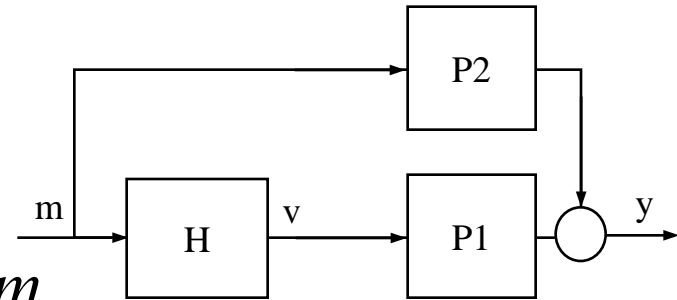
- General setting:

$$y = P_1 v + P_2 m = [P_1 H + P_2] m$$

$$\Rightarrow \min \| P_1 H + P_2 \|$$

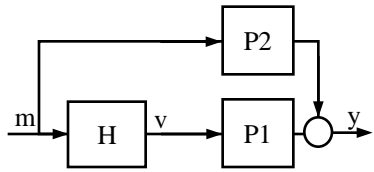
- If P_1 were invertible, $H = -P_1^{-1} P_2$

- Usually this is not the case

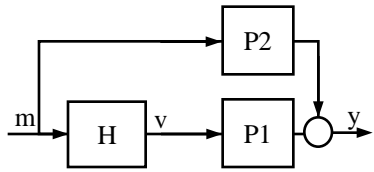


Feedback

and Feedforward Control



- Typical feedforward controller design:
 - separate invertible (outer) and non-invertible (inner) parts: $P_1 = P_{1o} P_{1i}$, $(P_{1i}^{-1} P_{1i} = I)$
 - Inner-outer factorization for multivariable systems, by inspection in SISO. Inner: all-pass (unity magnitude)
 - Solve the associated minimization problem
 - “By inspection” in SISO. Easy in 2-norm minimizing error variance for gaussian inputs. More complicated in inf-norm minimizing error energy for energy inputs.
 - Invert or approximate the inverse of the outer part



- Typical feedforward controller design (math)

- inner-outer factorization $P_1 = P_{1i}P_{1o}$, $(P_{1i}^{-1}P_{1i} = I)$
- minimization problem

$$\min \| P_1 H + P_2 \| = \min \| P_{1i} (P_{1o} H) + P_2 \| =$$

$$\min \| (P_{1o} H) + P_{1i}^{-1} P_2 \| \quad (\text{since } P_{1i}^{-1} P_{1i} = I \text{ and } \| P_{1i}^{-1} \| = 1)$$

1. $\| \cdot \|_2$: $H = (P_{1o})^{-1} (P_{1i}^{-1} P_2)^{-}$ (H2 - stable projection)

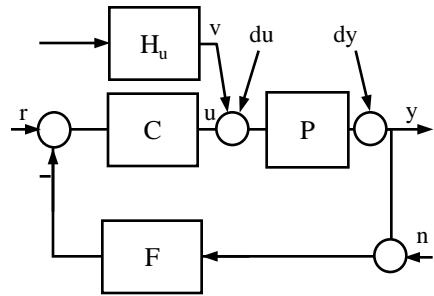
2. $\| \cdot \|_\infty$: $H = (P_{1o})^{-1} \{ \arg \min_X \| X + P_{1i}^{-1} P_2 \|_\infty \}$ (Hinf - Nehari)

If P_{1o} strictly proper, $(P_{1o})^{-1}$ is not well defined

(then, approximate, add weights, or regularize)

Feedback

and Feedforward Control



- Example of a (simplified) complete design:

- Heating a tube of water, 10liters, 0.1m diameter.

- Lumped model $mc_p \dot{T} = -hA(T - T_0) + q$

$$y = T, \quad u = q, \quad d = T_0$$

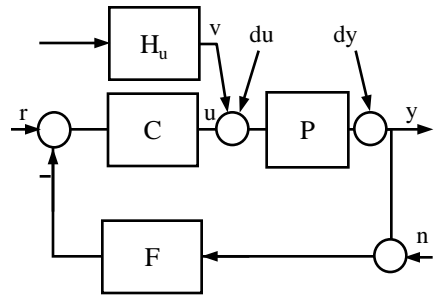
$$y = \frac{hA}{mc_p s + hA} d + \frac{1}{mc_p s + hA} u$$

- $mc_p \sim 40$, $h=5$, $A = \pi DL = 0.4$

- Also, suppose that T_0 is measurable and there is a 1sec delay in applying the control input ($u: q(t) = u(t-1)$), modeled by a 1st ord. Pade approximation

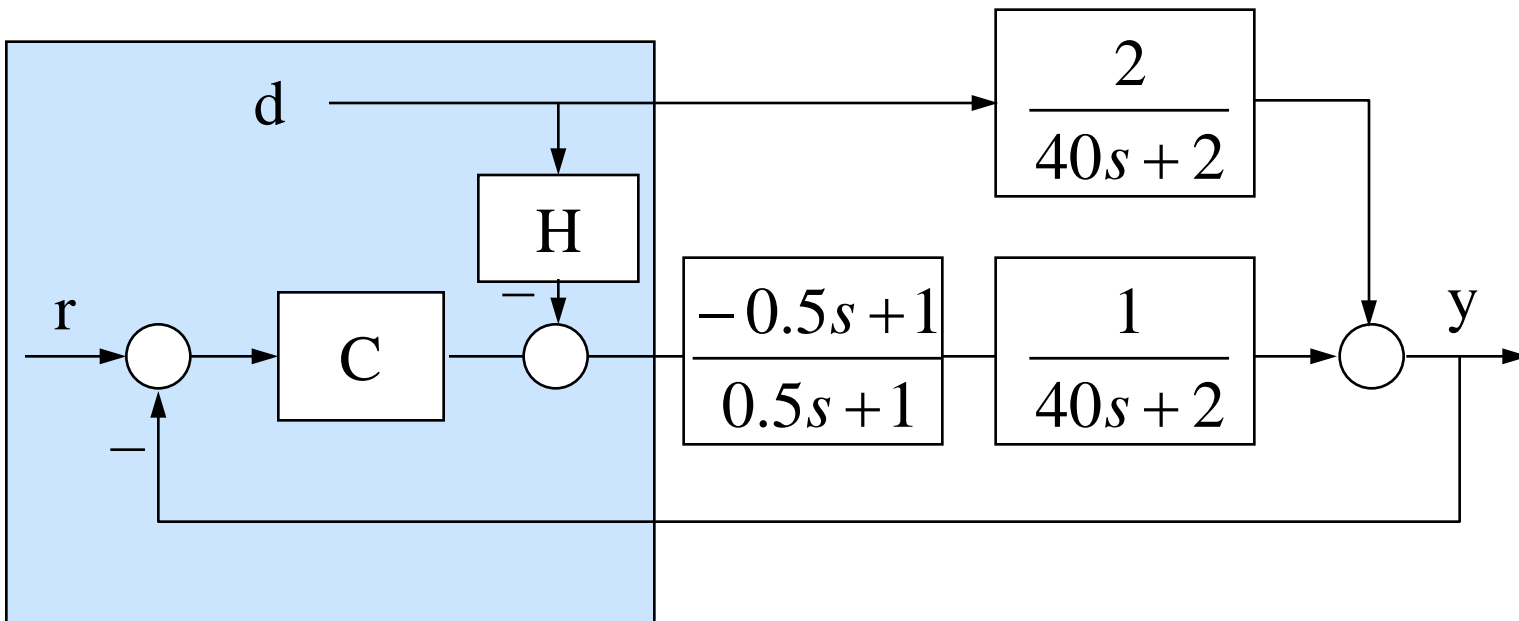
Feedback

and Feedforward Control



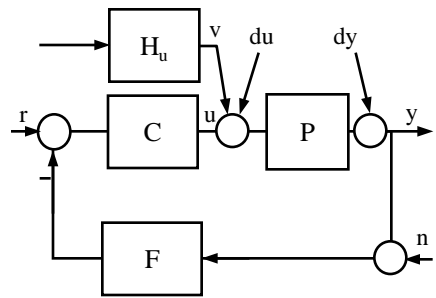
- Model
$$y = \underbrace{\frac{2}{40s+2}}_Q d + \underbrace{\frac{1}{40s+2} \frac{-0.5s+1}{0.5s+1}}_P u$$

- Feedback-feedforward controller

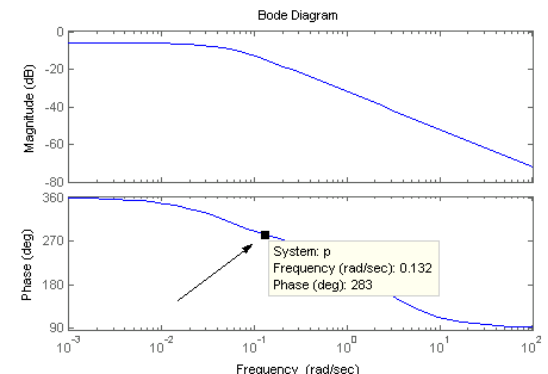


Feedback

and Feedforward Control

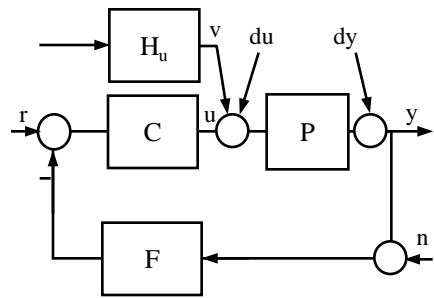


- Feedback controller tuning:
 - Choose $BW < 2$, e.g., 0.2 rad/s , (other design objectives and constraints would be included in this choice) \Rightarrow target crossover $0.2/1.5 = 0.133$
 - Plant transfer function and frequency response
 - $P = \text{tf}([-0.5 \ 1], [0.5 \ 1]) * \text{tf}(1, [40 \ 2])$
 - `bode(P)`
 - phase at crossover: -77°



Feedback

and Feedforward Control



- Feedback controller tuning:

- PI controller: $C = K(s+a)/s$.

- Adds phase at crossover: $\tan^{-1}(0.133/a) - 90^\circ$

- For 50° phase margin, $\tan^{-1}(0.133/a) = 37^\circ$

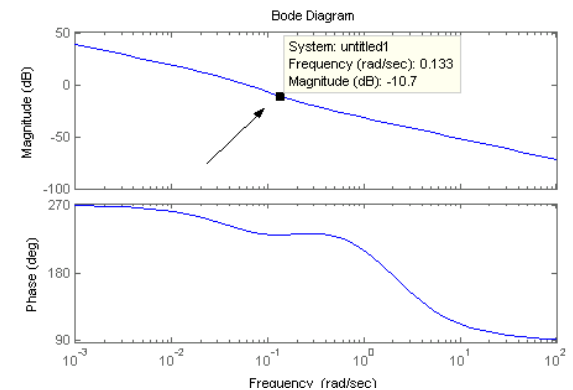
$$\Rightarrow a = 0.1765$$

- Find corresponding gain K:

- $C = \text{tf}([1 \ 0.1765], [1 \ 0]); \text{bode}(P * C)$

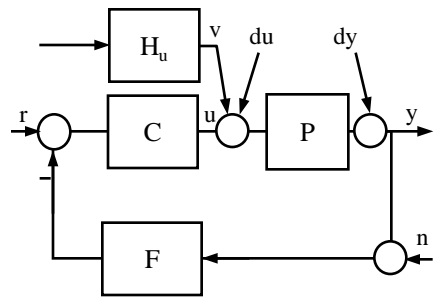
- evaluate magnitude at 0.133

- $\Rightarrow K = 3.43$



Feedback

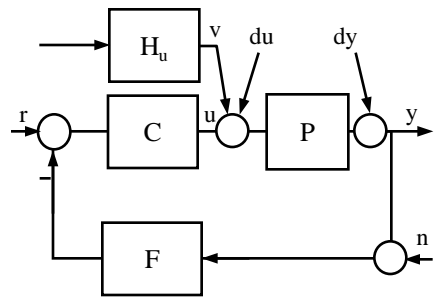
and Feedforward Control



- Feedback controller tuning:
 - Final controller: $C = \text{tf}([3.43 \ 0.61], [1 \ 0])$
 - Check step response and bandwidth
 - $\text{step}(\text{feedback}(P * C, 1)) \rightarrow 23\% \text{ overshoot}$
 - $\text{bode}(\text{feedback}(P * C, 1)) \rightarrow 0.2 \text{ rad/s bandwidth}$
 - sampling time $< 1/0.2/10$, ($\omega T/2 < 0.1$) say 0.1 s
 - control signal limits $0-1000 \text{ (W)}$

Feedback

and Feedforward Control



- Feedforward control

- Develop expressions

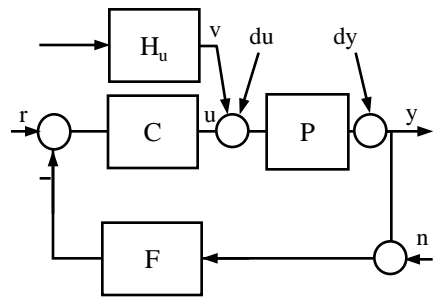
$$y = SPCr - SPHd + SQd \Rightarrow H : \min_H (\| SPH - SQ \|)$$

Subtract the feedforward signal to obtain the standard minimization problem

- Frequency weighting and control penalty

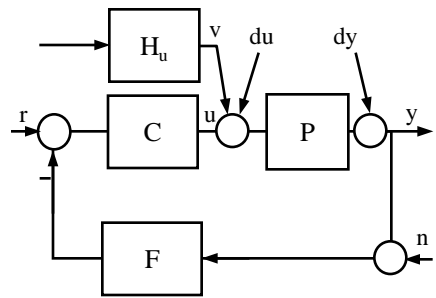
$$H : \min_H \left\| \begin{bmatrix} WSP \\ \rho I \end{bmatrix} H - \begin{bmatrix} WSQ \\ 0 \end{bmatrix} \right\|$$

- $W = \text{tf}([.5 \ 1], [1 \ 1e-4]); \rho = 1e-3$ % This W improves low-frequency performance; the control penalty $\rho \ll 1$, avoids ill-posed problems; larger values yield smoother controls



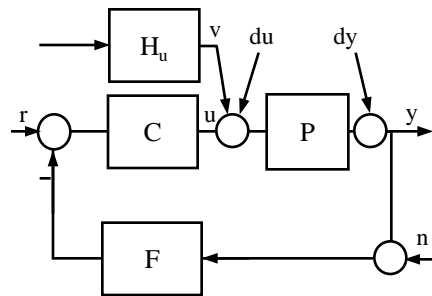
• Feedforward control computations

- `S=feedback(1,P*C); SP=feedback(P,C); SQ=Q*S;`
- `% Use the “feedback” function instead of just algebra`
- `G=[W*SP;r]; WT=([W*SQ;0]);`
- `[SPi,SPip,SPo]=iofr(ss(G)); Stil=inv([SPi,SPip]);`
- `R=minreal(Stil*WT);`
- `% Inner-outer factorization, minimal realization to keep system order low`
- `X2=stabproj(R-R.d)+R.d; H2o=minreal(inv(SPo)*[1 0]*X2);`
- `% Solve the associated net H-2 minimization problem but keep the throughput R.d in the stable part instead of splitting it (default in “stabproj”)`



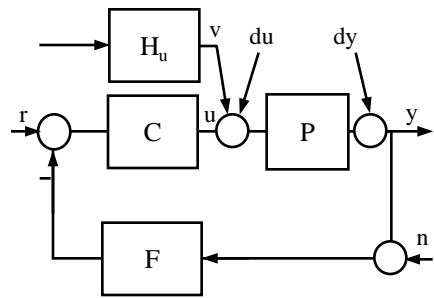
- computations continued

- `cut=sum((abs(eig(H2o))<1e-2));`
- `[H2s,H2f]=slowfast(H2o-H2o.d,cut);H2f=H2f+H2o.d;`
- `[a,b,c,d]=h_sysred(H2f,[],[]); H2=ss(a,b,c,d);`
- % Perform model reduction (the price of generality). “slowfast” to remove irrelevant slow modes. “h_sysred” is a custom function, based on balanced truncation. Works with the old state-space format.
- % Details in “Stability, Controllability, Observability notes,” <http://www.fulton.asu.edu/~tsakalis/notes/sco.pdf>



• H-inf computations

- minimizes the worst case; but the solution is more complicated -the so called 2-block problem with gamma-iteration. “nehari” solves the H-inf problem; it is a custom program with the (older) state-space format.
- `gmax=norm(WT,inf); gmin=norm(R(2),inf);`
- `while gmax-gmin>0.001`
- `gam=(gmax+gmin)/2; r0=(sfl(minreal(R(2))/gam))*gam;`
- `r1=minreal(R(1)*inv(r0));[a,b,c,d]=nehari(r1.a,r1.b,r1.c,r1.d,0);qm=ss(a,b,c,d);`
- `q=minreal(inv(SPo)*qm*r0); gtest=norm((r(1)-qm)*inv(r0),inf);`
- `if gtest < 1; gmax=gam; else gmin=gam;end`
- `end`
- `cut=length(find(abs(eig(q))<1e-2));[qs,qf]=slowfast(q-q.d,cut);qf=qf+q.d;`
- `[a,b,c,d]=h_sysred(qf,[],[]); Hi=ss(a,b,c,d);`



- Feedforward control implementation

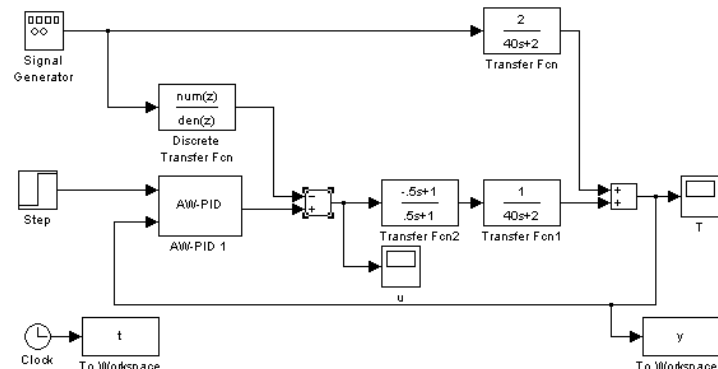
- Discretize the filter

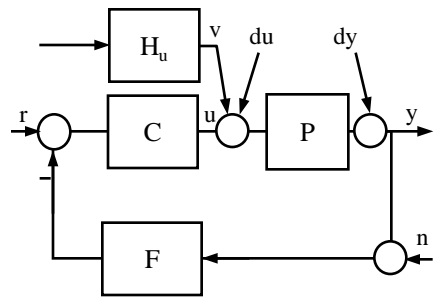
- `[nu,de]=tfdata(bilin(H2,1,'bwdrec',.1),'v')`

- `[nu,de]=tfdata(c2d(H2,.1,'tustin'),'v')`

- % use “bilin” with ‘bwdrec’ option or “c2d” with ‘tustin’

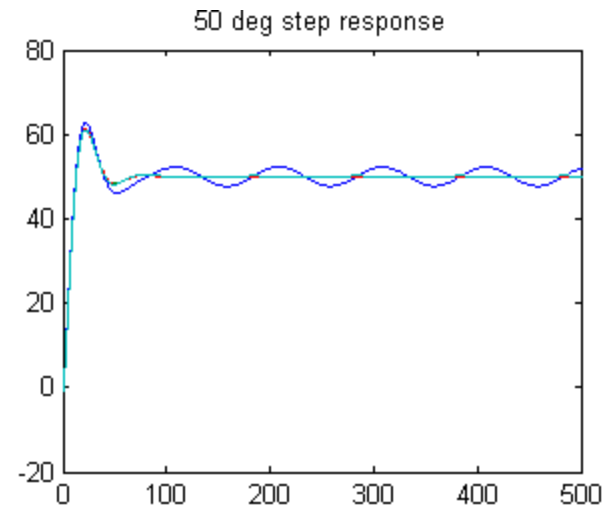
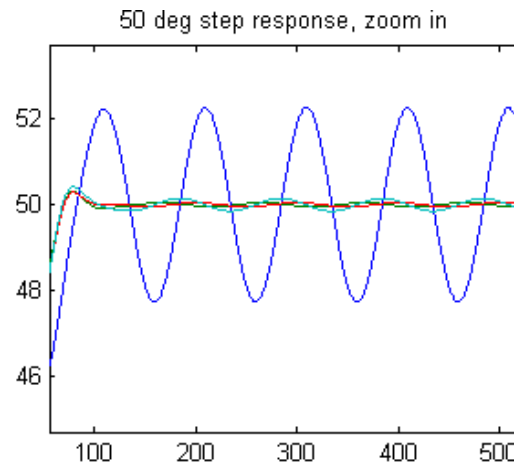
- Introduce the filter in the Simulink model

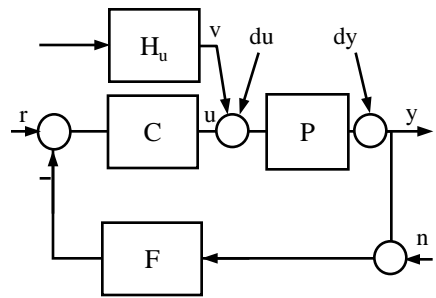




- Feedback and Feedforward control testing

- No feedforward (blue),
- H2 solution (red),
- Simple choice $H=2$ (cyan)



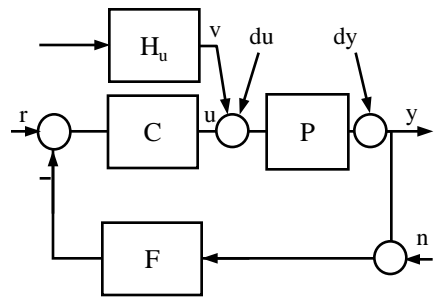


- **Feedback**

- Stabilizes or improves stability margin
- Reduces sensitivity to unknown perturbations and model imprecision
- Requires good sensors of process output

- **Feedforward**

- Leaves sensitivity and stability unaffected
- Provides faster corrections (than feedback)
- Requires good models and good sensors of disturbance



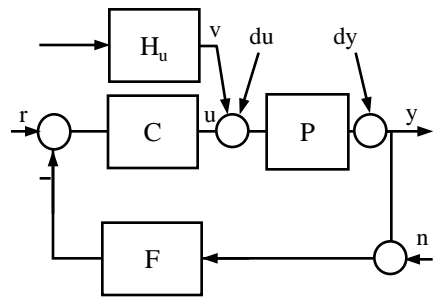
• Other Design Methods

– Feedback

- Linear Quadratic Regulator (LQR) methods
- General H_2 and H_{∞} solutions to weighted sensitivity minimization (more complicated problem statement)
- Model Predictive Control (MPC, on-line solution of an LQR optimization problem)
- Other heuristic, optimization-based methods (e.g., PID)

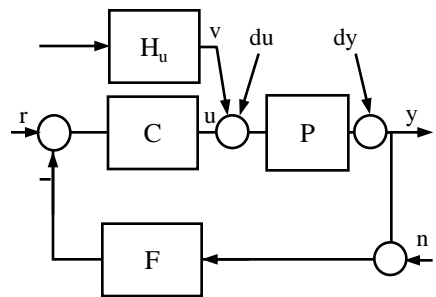
– Feedforward

- Heuristic, algebraic
- ### – Discrete-time (sampled data) solutions



• References

- Anderson-Moore (LQR),
- Zhou, Macejowski (Hx, model reduction, feedforward),
- Francis (Hx fundamentals),
- McFarlane-Glover (Coprime factor methods)
- Glad-Ljung (Linear/nonlinear/MPC... excellent survey)
- Astrom (PID control)



PID Control

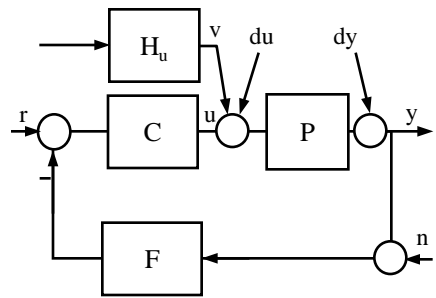
- PID Tuning

- PID is the industry workhorse

$$u = K_p e + K_i \int e + K_d \frac{de}{dt}$$

- Proportional, Integral, and Derivative action to achieve all the basic feedback objectives: adjust bandwidth, introduce phase lead for stabilization, increase gain at low frequencies for disturbance attenuation

PID Control



- PID Tuning

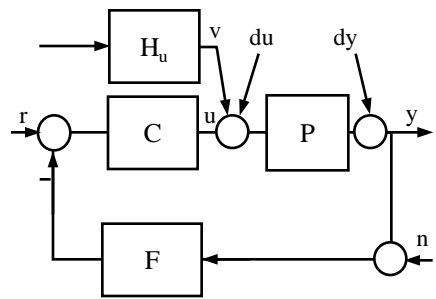
- Pseudo-differentiator: more realistic and avoids numerical problems in the design

$$u = K_p e + K_i \int e + \frac{K_d}{T} (e - v)$$

$$T\dot{v} = -v + e$$

- Transfer function:

$$\begin{aligned} C(s) &= K_p + \frac{K_i}{s} + \frac{K_d s}{Ts + 1} \\ &= \frac{(K_d + TK_p)s^2 + (K_p + TK_i)s + K_i}{s(Ts + 1)} \end{aligned}$$

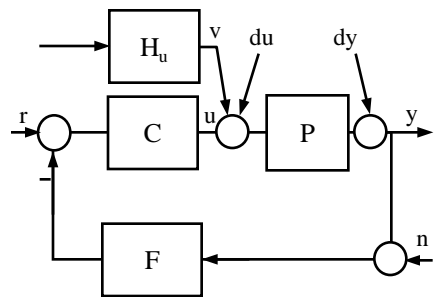


PID Control

- PID Tuning

- Choosing T : minimum value is the sampling time for discrete implementation. It does not affect the design very much as long as $1/T > 10 \text{ BW}$
- Tuning the PID: choosing the gain and the two zeros in the numerator (the num. is a 2nd degree, arbitrary polynomial, the den. is fixed)

- Typically, the two zeros are chosen the same $PID = \frac{K(s+a)^2}{s(Ts+1)}$
- PI: a special lag compensator $PI = \frac{K(s+a)}{s}$
- PD: a lead compensator $PD = \frac{K(s+a)}{(Ts+1)}$



PID Control

- PID Tuning

- Classical theory

- phase margin at the intended crossover

- Ziegler-Nichols

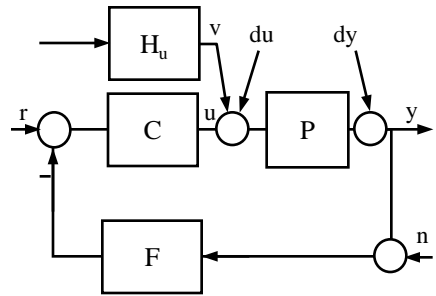
- Practical methods based on simple models

- Optimization and Loop-shaping

- MATLAB custom function “pidqtune” minimizes the distance from a desirable target; target selected using LQR theory so that the closed loop is at least feasible

- files in <http://www.fulton.asu.edu/~tsakalis/notes>

PID Control



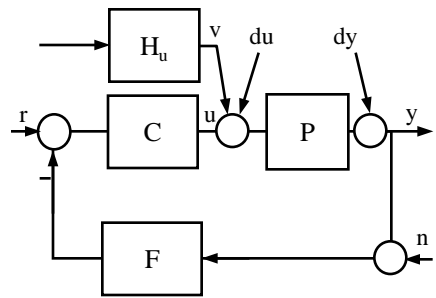
- Ziegler-Nichols rules
- From step response data:
 - R = effective slope (e.g., 5%-15%)
R ~ bandwidth
 - L = delay
- Experimentally, based on ultimate sensitivity:

Note: Z-N tunings are such that the ideal PID (with $\tau = 0$) has a double zero, i.e., $K_p^2 = 4K_iK_d$.

| <u>1</u> | P | PI | PID |
|----------------------|------|----------------------|---------------------|
| K_p | 1/RL | 0.9/RL | 1.2/RL |
| K_i | - | 0.27/RL ² | 0.6/RL ² |
| K_d | - | - | 0.5/R |

| <u>1</u> | P | PI | PID |
|----------------------|-------------------|------------------------------------|------------------------------------|
| K_p | 0.5K _u | 0.45K _u | 0.6K _u |
| K_i | - | 0.54K _u /P _u | 1.2K _u /P _u |
| K_d | - | - | 0.075K _u P _u |

PID Control



- PID Discrete Implementation

$$u_k = K_p e_k + K_i s_k + K_d (e_k - e_{k-1})$$

$$s_{k+1} = s_k + e_k$$

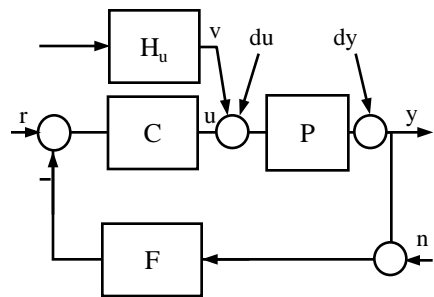
several different but equivalent implementation equations,

e.g., $\Delta u_k = u_{k+1} - u_k = \dots$

- Integrator windup

- Nonlinear behavior when the control input saturates (can lead to instability)
- Remedy: Anti-windup modification (limited integrators)

$$s_{k+1} = \min\left[\max\left\{s_k + e_k, \frac{u_{\min}}{K_i}\right\}, \frac{u_{\max}}{K_i}\right]$$



Controller Discretization

- Discretization

Continuous Time

$$\dot{x} = Ax + Bu$$

$$y = Cx + Du$$

$$\frac{y(s)}{u(s)} = G(s) = D + C(sI - A)^{-1} B$$

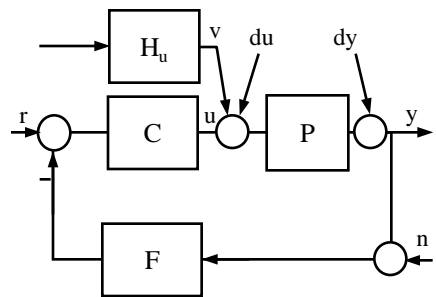
Discrete Time

$$x_{k+1} = Ax_k + Bu_k$$

$$y_k = Cx_k + Du_k$$

$$\frac{y(z)}{u(z)} = G(z) = D + C(zI - A)^{-1} B$$

- MATLAB: “bilin” with ‘bwdrec’ (backward rectangular), ‘fwdrec’, ‘tustin’, etc.
- “c2d” function for system objects, with ‘zoh’ (zero order hold) option, etc.



Controller Discretization

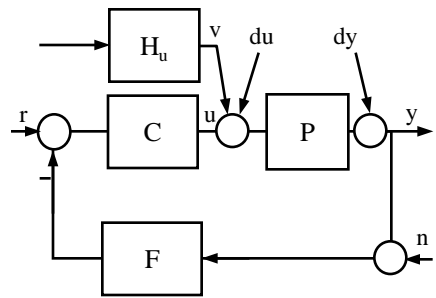
- Discretization derivations

Forward Euler $\dot{x} = Ax + Bu \rightarrow \frac{x_{k+1} - x_k}{T} = Ax_k + Bu_k$

$$G(z) = D + C[zI - (I + AT)]^{-1}TB$$

Backward Euler $\dot{x} = Ax + Bu \rightarrow \frac{x_k - x_{k-1}}{T} = Ax_k + Bu_k$

$$\begin{aligned} G(z) &= D + C[zI - (I - AT)^{-1}]^{-1}(I - AT)^{-1}TBz \\ &= D + C[zI - (I - AT)^{-1}]^{-1}\{z \pm (I - AT)^{-1}\}(I - AT)^{-1}TB \\ &= [D + C(I - AT)^{-1}TB] + C(I - AT)^{-1}[zI - (I - AT)^{-1}]^{-1}(I - AT)^{-1}TB \end{aligned}$$



Controller Discretization

- Discretization derivations

ZOH equivalent

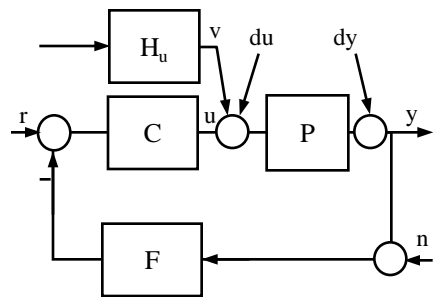
(sampled data response with piecewise constant inputs) :

$$\dot{x} = Ax + Bu \rightarrow x(t+T) = e^{AT} x(t) + \int_t^{t+T} e^{A(t+T-\tau)} Bu(\tau) d\tau$$

$$\rightarrow x_{k+1} = \{e^{AT}\} x_k + \{A^{-1}(e^{AT} - I)B\} u_k, y_k = Cx_k + Du_k$$

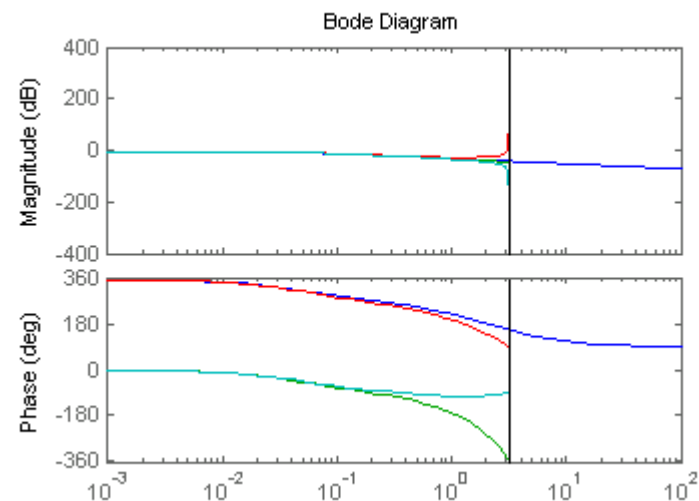
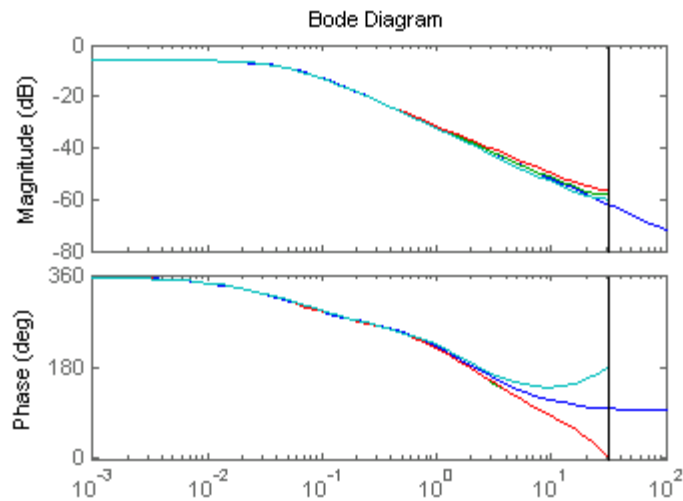
Tustin :

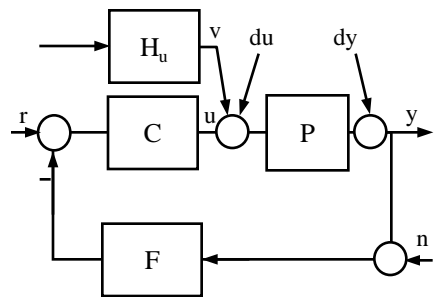
$$s = \frac{2}{T} \frac{z-1}{z+1}, \left(z^{-1} = e^{-sT} \stackrel{\text{Pade}}{=} \frac{1-sT/2}{1+sT/2} \Rightarrow s = \dots \right)$$



Controller Discretization

- Comparison of different discretizations
 - essentially the same results up to an order of magnitude below sampling rate (see bode plots below, $T_s = 0.1, 1$)
 - Slower sampling rates require either careful selection of discretization method or discrete design altogether



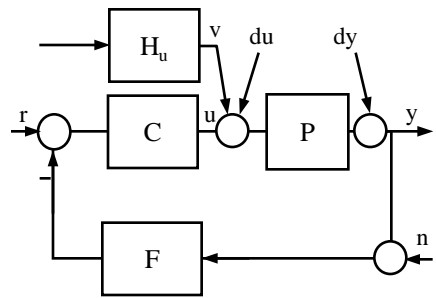


Controller Discretization

- Discretization comments

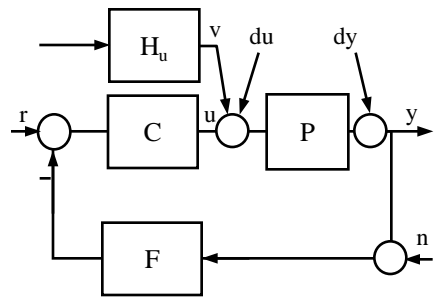
- Continuous time design: done once, discretized easily for different sampling times (T_s) -by any method.
- When approaching the sampling frequency, the discretized systems start deviating “unpredictably” from the continuous time frequency response and from each other
- In such a case, there is no guarantee that a controller/filter will work as expected (e.g., discretizing a slow system with a slow sampling rate but asking for a very fast response)

Controller Discretization

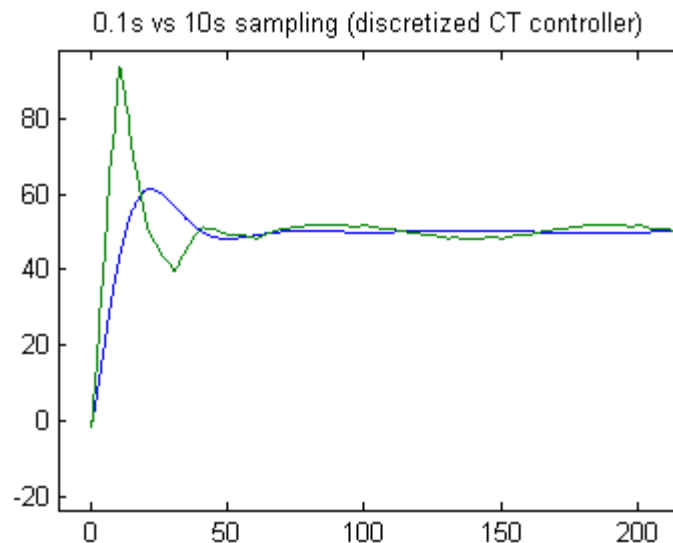


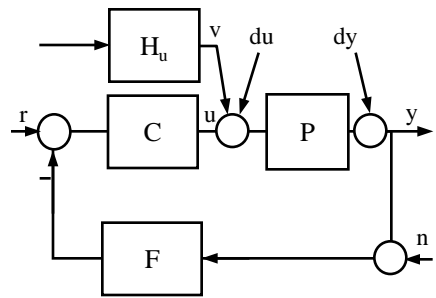
- Remedy: Obtain the ZOH equivalent response of the system and design a discrete controller/filter using the equivalent DT techniques (similar to CT but different computations)
- To illustrate the process, let us repeat the previous exercise (water tube) but with a 10sec sampling time
 - The system time constant is 20sec, so this discretization is somewhat adequate to describe the open loop. But the required closed-loop bandwidth is 0.2, (~5sec time constant) and therefore the sampling is too coarse to approximate the continuous time response.

Controller Discretization



- Using the previous (CT) design and discretizing the controller at 10sec, the closed-loop is unstable for ZOH and forward Euler discretization and stable for backward Euler; even for this, the response differs considerably from the continuous time design





Controller Discretization

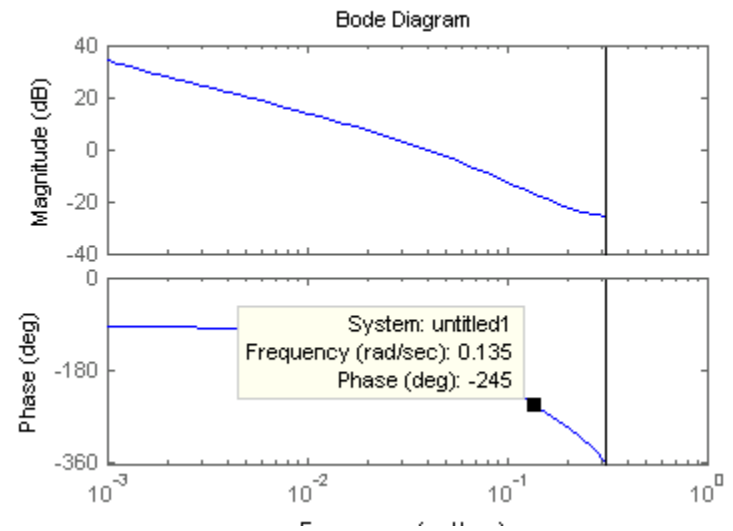
- Redesign the discrete PI(D) controller $K(z+a)/(z-1)$
- $Pd = c2d(P,10) = (0.1812 z + 0.01555)/(z^2 - 0.6065 z)$
- Let $C = tf(1,[1 -1],10)$, and get $bode(Pd*C)$

- At crossover, phase = -245°
- Need 115° phase lead from $z+a$

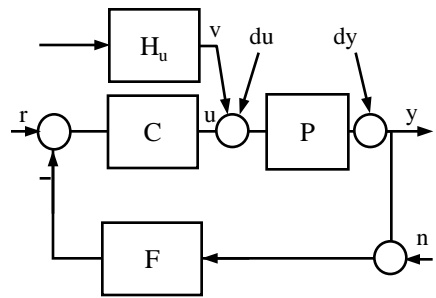
$$a = \frac{\sin(0.133*10)}{\tan(115\pi/180)} - \cos(0.133*10)$$

$$= -0.6913$$

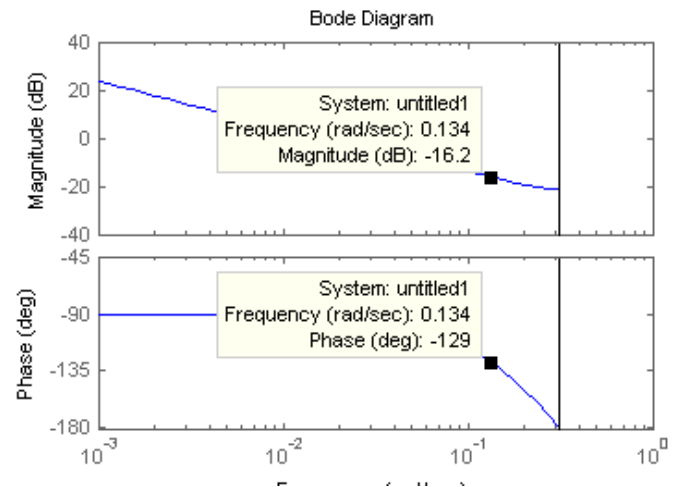
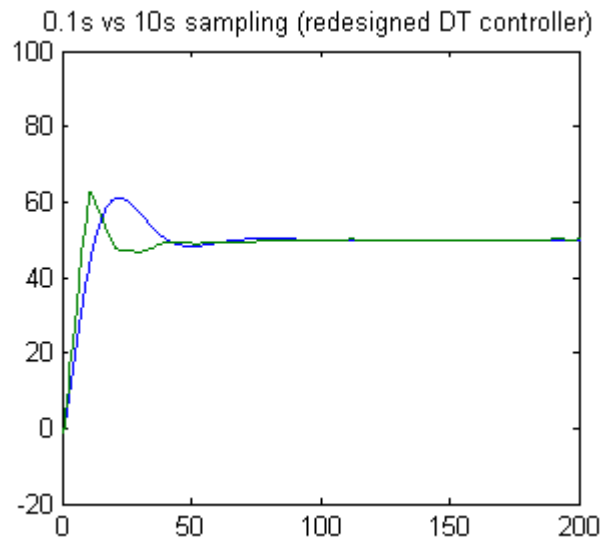
- Adjust $C = tf([1 -.6913],[1 -1],10)$
- and re-compute bode to find the gain K

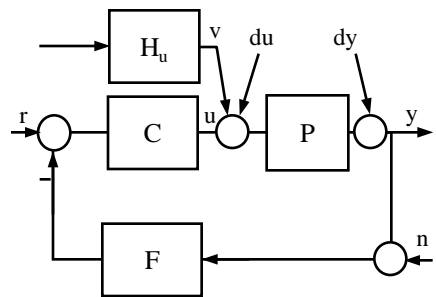


Controller Discretization



- We need $K = 10^{(16.2/20)} = 6.456$ to have 0.13 as the crossover frequency (with 50° phase margin). So,
- $C = \text{tf}(6.456 * [1 \ -0.6913], [1 \ -1], 10)$
- Good feedback performance!

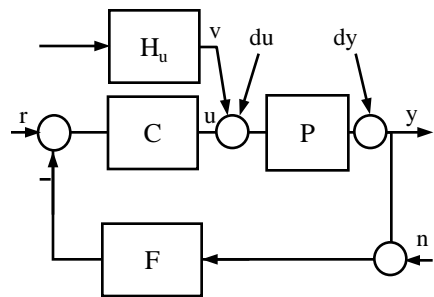




Controller Discretization (alt.)

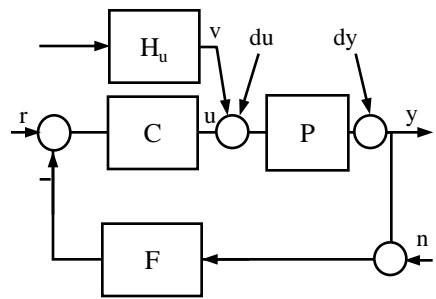
- An alternative to the complete DT redesign is to adjust the CT PID for the phase lag of the ZOH at crossover ($\sim \omega T/2$) and then discretize using the Tustin transformation to preserve the CT frequency response; the method works well as long as the crossover is well-below the Nyquist frequency.
- At crossover, the ZOH lag is approx. 0.665rad, or 38deg; design C for PM = 50+38 deg $\Rightarrow C = (5.504 s + 0.1956)/s$
- Discretize at 10 sec (Tustin) ; $D = c2d(c1,10,'tustin') \Rightarrow$

$$D = (6.482 z - 4.526)/(z-1)$$
 (very close to the fully DT design)



Controller Discretization

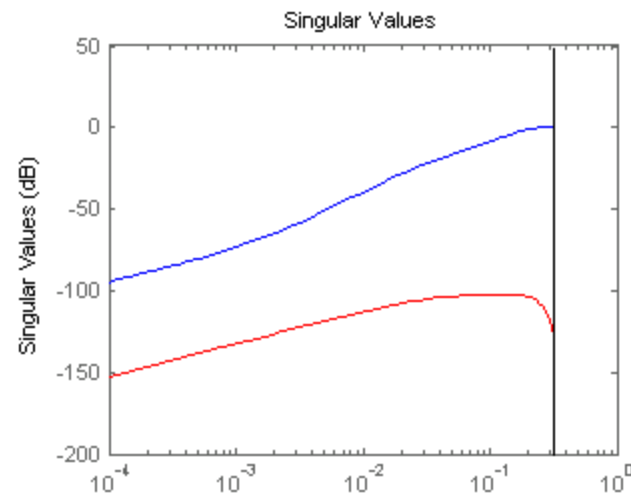
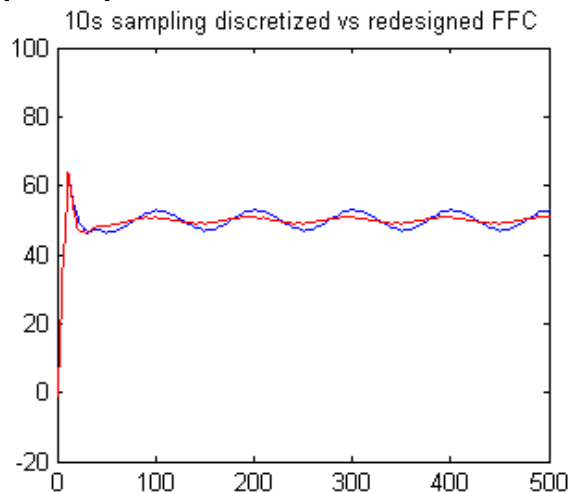
- Also need to redesign the FFC
 - The procedure is similar:
 - Discretize (ZOH equivalent) the plant model and form the various systems
 - Apply Tustin bilinear transform (norm preserving) to get a continuous-time equivalent problem
 - Solve for the FFC as before
 - Recover the discrete time solution by the inverse Tustin transform.



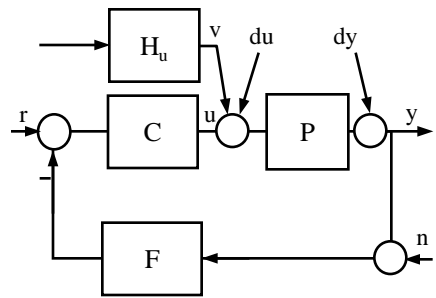
Controller Discretization

- DT-FFC results

- The redesigned DT FFC response (blue) shows significant improvement over the 10sec discretization of the CT solution (red)
- But even though the error singular value plot is very small (red), the disturbance effect is not negligible...

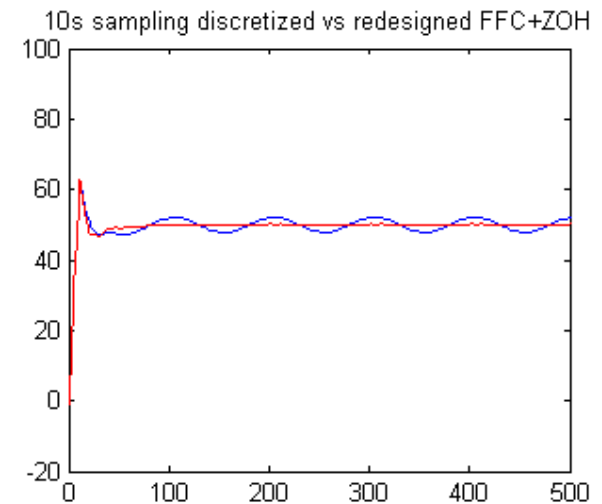


Controller Discretization



- DT-FFC results

- The explanation is that the DT solution is accurate (no “unstable” zeros) but only for piecewise constant inputs in 10sec intervals. Our disturbance is a continuous sinusoid.
- Indeed, when adding a ZOH after the disturbance source, the DT redesigned FFC works very well while the CT discretized does not.
- Unfortunately real disturbances are not ZOH-sampled and lower sampling rates are detrimental to controller performance



Model Identification

- Parametric Model Identification from I/O data.
 - Non-parametric vs. Parametric models
 - Model parameterization: $y = P[u;\theta]$
 - Estimation error (to be minimized)
 - Batch/Recursive update equations
- For more details: Notes on adaptive algorithms, http://www.eas.asu.edu/~tsakalis/notes/ad_alg.pdf
- other bibliography: Ljung, Soderstrom-Stoica, Ioannou-Sun, Goodwin-Sin

Model Identification



- Data conditioning (pre-processing): avoid estimation of uninteresting effects
 - High frequency filtering
 - Offset and Drift removal (low-frequency filtering)
 - Justified by linearization principles
 - Scaling/conditioning
 - Numerical Sensitivity, uncertainty interpretations
 - Speed of convergence in recursive algorithms
- SNR and record-length issues

Model Identification

- Model parametrization

$$\dot{x} = Ax + Bu; \quad y = Cx + Du; \quad \theta = [A, B, C, D]$$

$$x_{k+1} = Ax_k + Bu_k; \quad y_k = Cx_k + Du_k; \quad \theta = [A, B, C, D]$$

$$y_{k+1} = b_n u_k + b_{n-1} u_{k-1} + \dots + a_n y_k + a_{n-1} y_{k-1} + \dots; \quad \theta = [b_n, \dots, a_n]$$

- Models may include other external inputs such as noise, disturbances, effects of initial conditions (short data records/batch ID)
- Parsimonious models: independent parameters, minimal parameter count. Identifiability
- Persistent and Sufficient Excitation

Model Identification



- Parameter Estimation Objective
 - Estimation error formulation, equation error
 - $e = y - \phi^T \theta$; $\phi =$ regressor.
 - Linear-in-the-parameters (efficient algorithms exist)
 - Left factorization (observer), Coprime factor uncertainty
 - $e = y - P[u; \theta]$
 - Usually NonLinear-in-the-parameters
 - Additive uncertainty
 - ...

Model Identification



- Parameter Estimation Methods
 - Least-squares, exponential weighting/fading memory
 - Fast recursive algorithms, Ellipsoidal parameter uncertainty
 - RMS (asymptotic)
 - Simple gradient algorithms, ultra-fast execution, slow convergence
 - Min-max (L-inf)
 - Linear programming algorithms, non recursive (except for sub-optimal approximations), Polytopic parameter uncertainty

Model Identification

- Estimation algorithms

- Linear model estimation error $e_k = y_k - \phi_k^T \theta_k$

$$\text{Gradient: } \theta_{k+1} = \theta_k + \frac{P \phi_k e_k}{1 + \phi_k^T P \phi_k}, \quad P > 0$$

$$\text{Least-Squares: } \begin{cases} P_{k+1} = \frac{1}{\lambda} \left[P_k - \frac{P_k \phi_k \phi_k^T P_k}{\lambda + \phi_k^T P_k \phi_k} \right], & 0 < \lambda \leq 1 \\ \theta_{k+1} = \theta_k + P_{k+1} \phi_k e_k \end{cases}$$

- λ : exponential weighting (forgetting factor). Typical values 0.990-0.999; depends on the number of parameters, excitation properties, parameter variations with time, etc.

Model Identification

- Estimation algorithms, Kalman Filter
 - Given the model

$$x_{k+1} = A_k x_k + v_k$$

$$y_k = C_k x_k + n_k$$

where, $[v, n]$ is white noise with intensity $\text{diag}(Q, R)$

- An optimal (min variance) estimate of the state x is

$$\hat{x}_{k+1} = A_k \hat{x}_k + L_k (y_k - C_k \hat{x}_k)$$

$$L_k = A_k P_k C_k^T (C_k P_k C_k^T + R)^{-1}$$

$$P_{k+1} = A_k P_k A_k^T + Q - A_k P_k C_k^T (C_k P_k C_k^T + R)^{-1} C_k P_k A_k^T$$

Model Identification

- Kalman Filter details

- Assumptions: $R > 0$, (A, C) observable, (A, Q) controllable
- P-update: at steady-state becomes the discrete time filter algebraic Riccati equation. Its positive definite solution guarantees that $(A-LC)$ is stable.
- Returning to our estimation problem, write the linear model as a dynamical system $\theta_{k+1} = I\theta_k + v_k$, $y_k = \phi_k^T \theta_k + n_k$
- and apply KF

$$\hat{\theta}_{k+1} = \hat{\theta}_k + L_k (y_k - \phi_k^T \hat{\theta}_k), \quad L_k = P_k \phi_k (\phi_k^T P_k \phi_k + R)^{-1}$$

$$P_{k+1} = P_k + Q - P_k \phi_k (\phi_k^T P_k \phi_k + R)^{-1} \phi_k^T P_k$$

Model Identification



- Take $R=1$ (for a scalar output) and $Q \rightarrow 0$ to recover the standard LS updates
 - Some expressions may “look” different but they become identical after some algebraic manipulations
- Observability is equivalent to persistent excitation of ϕ
- The difference in implementation becomes important when adding constraints to parameters
- The KF handles parameter variations naturally through the noise term v and its covariance Q ; if desired an exponentially weighted formulation can be derived to obtain the previous expressions; although it is not equivalent, the effect is similar

Model Identification

- An alternative algorithm for System Identification: Concatenate parameters and states into a big model (still linear but time-varying) and apply KF
 - this requires the system description in an observable form (left factorization); its generality is justified as follows:

$$\begin{aligned}x_{k+1} &= Ax_k + Bu_k & \Rightarrow & x_{k+1} = Fx_k + \theta_1 y_k + \theta_2 u_k \\ &= (A - LC)x_k + LCx_k + Bu_k & y_k &= Cx_k + \theta_3 u_k \\ &= Fx_k + Ly_k + (B - LD)u_k\end{aligned}$$

$$y_k = Cx_k + Du_k$$

- F,C are design parameters: F should be stable and (F,C) should be observable

Model Identification

- Collect states and apply KF to estimate both states and parameters

$$\begin{bmatrix} x_{k+1} \\ \theta_{1,k+1} \\ \theta_{2,k+1} \\ \theta_{3,k+1} \end{bmatrix} = \begin{bmatrix} F & Iy_k & Iu_k & 0 \\ 0 & I & 0 & 0 \\ 0 & 0 & I & 0 \\ 0 & 0 & 0 & I \end{bmatrix} \begin{bmatrix} x_k \\ \theta_{1,k} \\ \theta_{2,k} \\ \theta_{3,k} \end{bmatrix}, \quad y_k = [C, 0, 0, u_k] \begin{bmatrix} x_k \\ \theta_{1,k} \\ \theta_{2,k} \\ \theta_{3,k} \end{bmatrix}$$

- Notice that the model is nonlinear in the states and parameters but it becomes linear if the output is measured (and becomes an external time-varying parameter).
- Drawback: output additive noise enters nonlinearly in this model
- Choose $Q_{11} \gg Q_{22}$ (states vary much faster than parameters)
- Convergence condition is again the persistence of excitation

Model Identification

- Other Issues

- Persistent excitation $\exists \delta, n > 0: \sum_{k=N}^{N+n} \phi_k \phi_k^T > \delta I > 0$, for all N
- Possible parameter drifts in the absence of sufficient excitation (noise can mask the system)
 - Various modifications: Parameter projection, dead-zone, regularization noise, excitation monitoring
- Modeling and estimation of dynamic uncertainty (region of model validity; analysis of residuals)

Model Identification

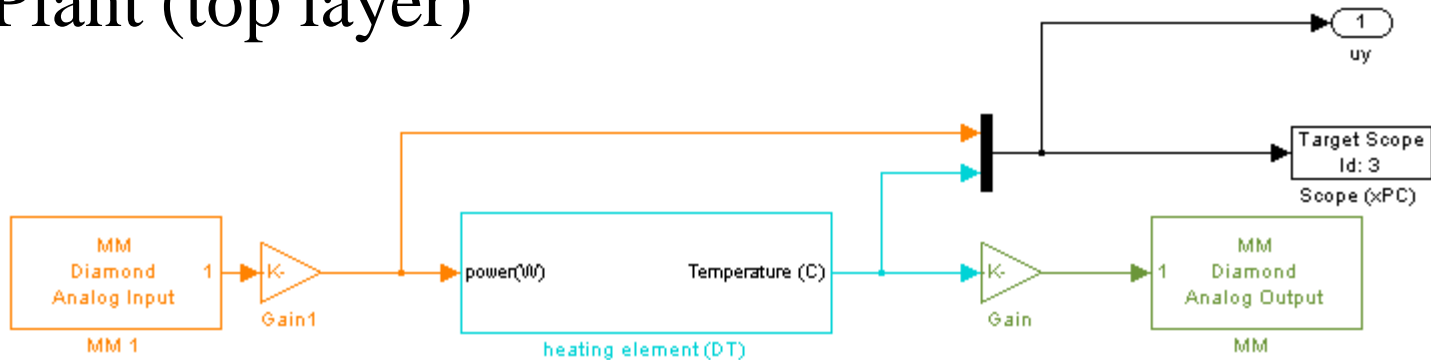


- Estimator modifications
 - Parameter projection
 - Knowledge of a convex set containing the parameters; find the best estimate in the set
 - Dead-zone
 - Do not update when the error is below the noise level
 - Regularization noise
 - Add artificial noise to the I/O pair used for estimation. Penalizes large estimates (\sim min norm solution), ensures covariance boundedness, at the expense of a small bias
 - Excitation monitoring (high level logic)

Model Identification

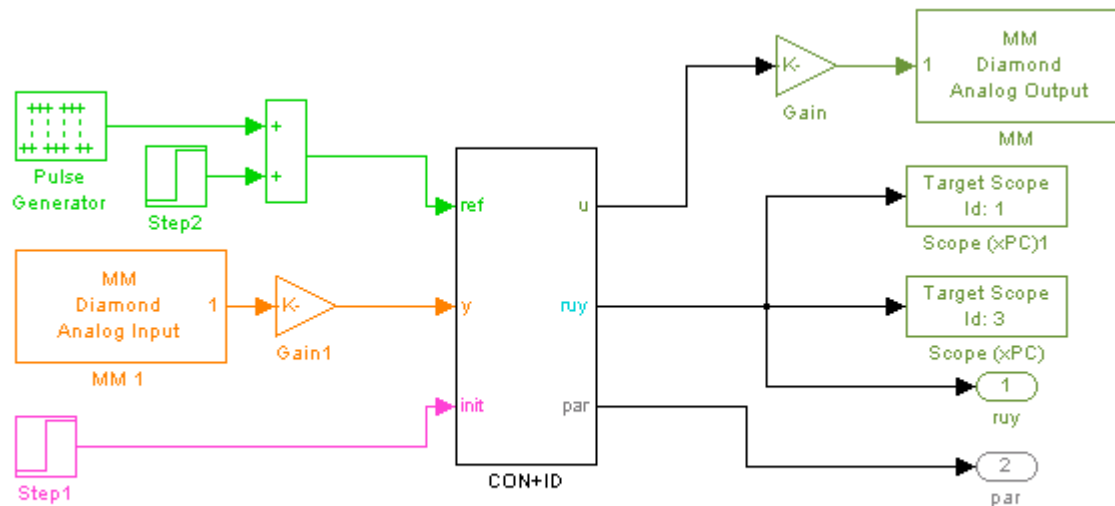
- Example

- Temperature control of a heating element with on-line identification of its transfer function (Experiment 5)
- Plant (top layer)



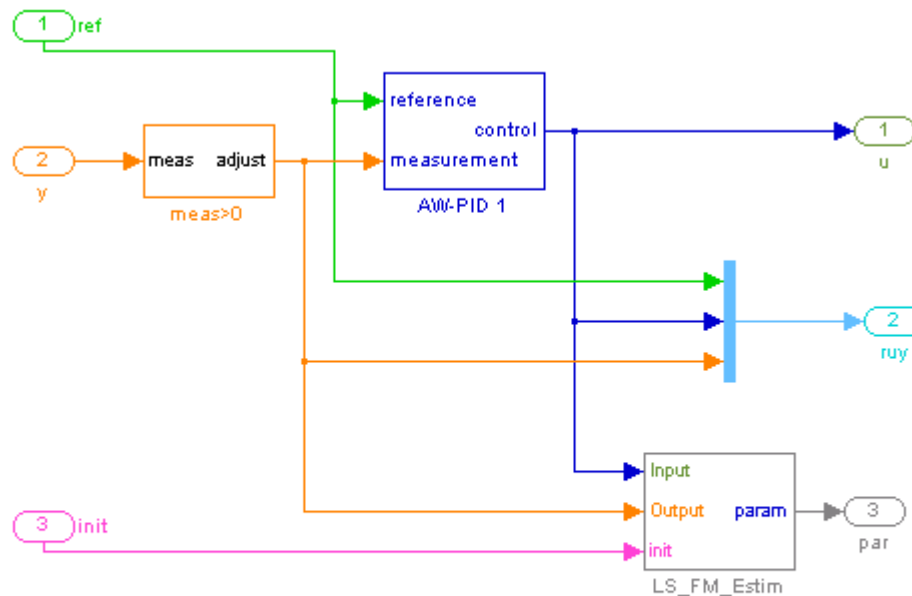
Model Identification

- Example
 - Controller (top layer)



Model Identification

- Example
 - Controller block: PID, LSE



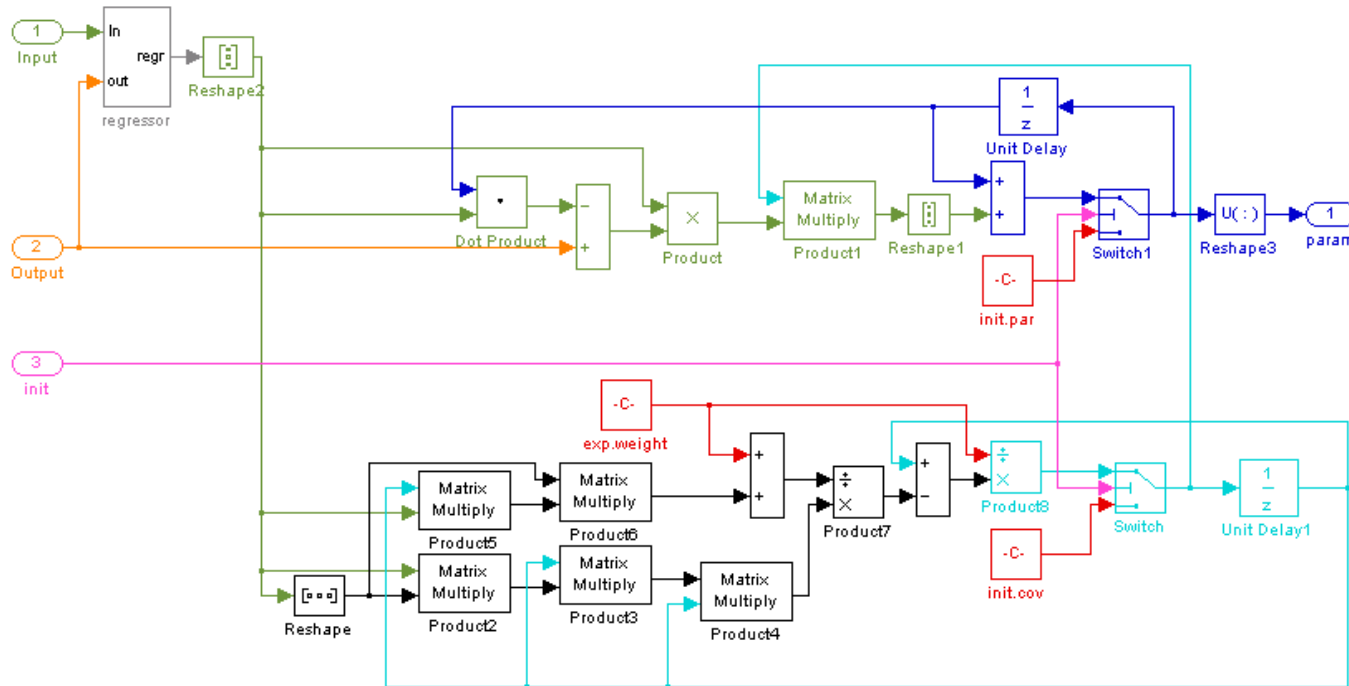
INITIALIZATION:

Tsa=.2;N=2;rho=1e3;lambda=.995;u_noise=1e-1;y_noise=1e0;

Model Identification

- Example

- Fading Memory Least Squares Estimator



Model Identification



- Example

- Experiment with different regularization noise levels, different estimators
 - LS parameter (textbook), LS/KF parameter (notes), KF parameter+state (notes)
- Get familiar with the embedded function block and analyze the impact on execution speed
- Try different model orders, add disturbances and monitor the excitation for different reference inputs...
- Use prefilters on I/O data to remove nonlinear DC bias from linearization

Model Identification



- Example
 - Supplied functions:
 - Various estimator blocks (in idblocks)
 - Code to extract the state-space or transfer function model from the parameter vector in comments inside each block; remember to adjust the code when changing the model order or model structure
 - exp6KF.mdl contains a non-real-time version of the simulator to illustrate the operation of the parameter estimators

Instrument Ratings



- Usually static characteristics from manufacturers
 - Sensitivity: output magnitude to unit input
 - Dynamic range: upper-lower limits. Often expressed as a ratio in dB, usually range/resolution
 - Resolution: smallest change that can be detected
 - Linearity: maximum deviation from straight line
 - Zero/full scale drift: drift when input is maintained steady for a long period

Accuracy-Precision



- Errors can be deterministic (systematic) or random
 - Measurement accuracy = closeness of the measured value to the true value
 - Instrument accuracy = worst case accuracy within the dynamic range
 - Precision = reproducibility or repeatability
 - precision = measurement range/error variance
 - precision \sim measurement variance for constant input

Significance in measurement and computations

- Is a measurement 0.1V the same as 100mV?
Or, is a resistance value $4.7\text{k}\Omega = 4700\Omega$?
What is the current flowing through a $3.3\text{k}\Omega$ resistor when the voltage is 1.0V?
- Unless otherwise specified, the value is accurate to within 1 (or 1/2) least significant digit. So,
 - $0.1\text{V} = 0.1\text{V} \pm 0.1\text{V}$
 - $100\text{mV} = 100\text{mV} \pm 1\text{mV} = 0.100\text{V} \pm 0.001\text{V}$

Significance in measurement and computations

- In computations, the answer should have the same significant digits as the least of the numbers used in the calculation:
 - Current = Voltage / Resistance = $(1.0 / 3.3\text{k})\text{A} =$
from computation $(0.3030\dots\text{m})\text{A} = 0.30\text{mA}$
 - Significant digits: digits past first nonzero digit
 $1.0\text{V}/3300\Omega = (0.0003030\dots)\text{A} = 0.00030\text{A}$
 - **Note:** calculators compute with a fixed number of digits. Scientific notation is consistent with the significant digit concept.

Sensors and Actuators



- Sensors:
 - “Process Variable” to “Data” conversion
 - Change in certain material properties with changes in a process variable
 - Variety of sensor outputs: Electrical (potentiometers, thermocouples, thermistors, strain gauge), mechanical (bi-metallic thermometers), numeric (counters, optical sensors)

Examples of Sensors and Actuators

- Actuators:
 - “Data” to “Process manipulated variable” conversion
 - Variety of actuator inputs: Electrical (analog control circuits), numeric (computer control systems), pneumatic (some industrial controls)
 - Actuators/Final Control Elements: Heater (electric coil, gas burner, steam flow), Valve (pneumatic, solenoid, motor-driven), Light, Relay, Switch

- Sensor Signal Conditioning
 - Convert signals to a form suitable for interfacing with the other elements of the process control loop
 - Digital form: advantages in computations, maintenance, reliability, cost
 - Typical operations: Amplification, Linearization, Filtering and Impedance Matching

Sensors: Signal Conditioning



- Type of signal (variation/range) is usually fixed, depending on physical properties, (e.g., changes in resistance, voltage, etc).
- Amplification: Adjust the usually low signal level. Input impedance (transfer function) is important to assess speed of sensor response
- Linearization: Usually required; mild to severe nonlinearities; look-up tables and fitting functions; accuracy vs. precision

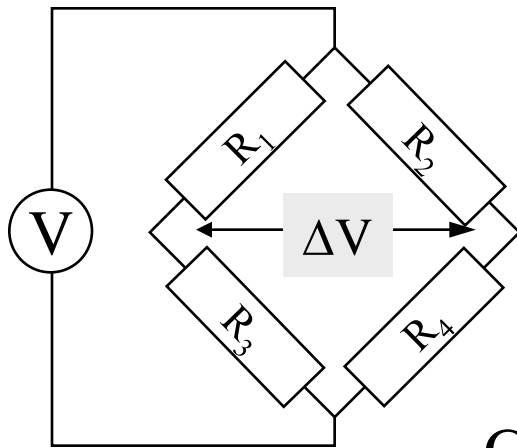
Sensors: Signal Conditioning



- Signal Conversion example: change in resistance to change in voltage or current
- Bridges to handle small fractional changes in resistance
- Analog Filtering to reduce aliasing effects.
- Impedance matching to improve dynamics and sensor signal strength (a power transfer problem)
- Active or passive filters; input impedance considerations

Sensors: Signal Conditioning

- Wheatstone bridge, current balance bridge: detection of a null condition (irrespective of voltage drifts)

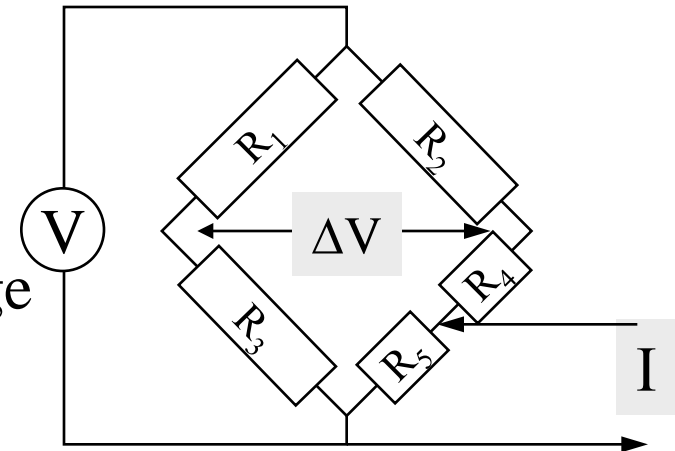


$$\Delta V = V \frac{R_2 R_3 - R_1 R_4}{(R_1 + R_3)(R_2 + R_4)}$$

Current balance bridge

$$I \text{ s.t. } \Delta V = 0$$

$$R_4 \gg R_5$$



Thermal Sensors

- Thermal Energy ~ atom vibrations, atom speed
 - Average energy per molecule
 - Different Scales (K,C and R,F)
 - Thermal Energy of one molecule
 - $\frac{3}{2} kT$, $k = 1.38 \cdot 10^{-23} \text{ J/K}$ (Boltzmann)
 - Average thermal speed $\sqrt{\frac{3kT}{m}}$
 - O_2 , 90F, $v = 488\text{m/s}$
- Key sensor property: resistance vs Temperature

Thermal Sensors

- Metal resistance increases with temperature (more electron collisions).
 - Resistance Temperature Detector (RTD)
 - Pt: almost linear in $[-100, 600]$, repeatable, $0.004/^\circ\text{C}$ sensitivity.
 - Ni: nonlinear, less repeatable, $0.005/^\circ\text{C}$ sensitivity
 - measurement with a bridge
 - response: time for wire to acquire temperature
 - self heating effect from power supply ($\sim 1^\circ\text{C}$)

Thermal Sensors



- Semiconductor resistance decreases with temperature (more free electrons): Thermistors
 - highly nonlinear resistance variation with temp.
 - effective range $[-100, 300]$ °C
 - Insensitive at high temperatures
 - 0.5-10s response time (depending on sensor mass and environment)
 - encapsulation material issues

Thermal Sensors

- Thermocouples: thermo-electric effect in a junction of different metals, voltage generation vs. temperature
 - Require cold junction reference
 - Almost linear; linearization tables for accuracy
 - Good range, sensitivity, inertness
 - Type J: $[-200, 700]^{\circ}\text{C}$, $0.05\text{mV}/^{\circ}\text{C}$, max 43mV
 - Type K: $[-190, 1260]^{\circ}\text{C}$, max 55mV
 - Type R: $[0, 1482]^{\circ}\text{C}$, $0.006\text{mV}/^{\circ}\text{C}$, max 15mV

Thermal Sensors



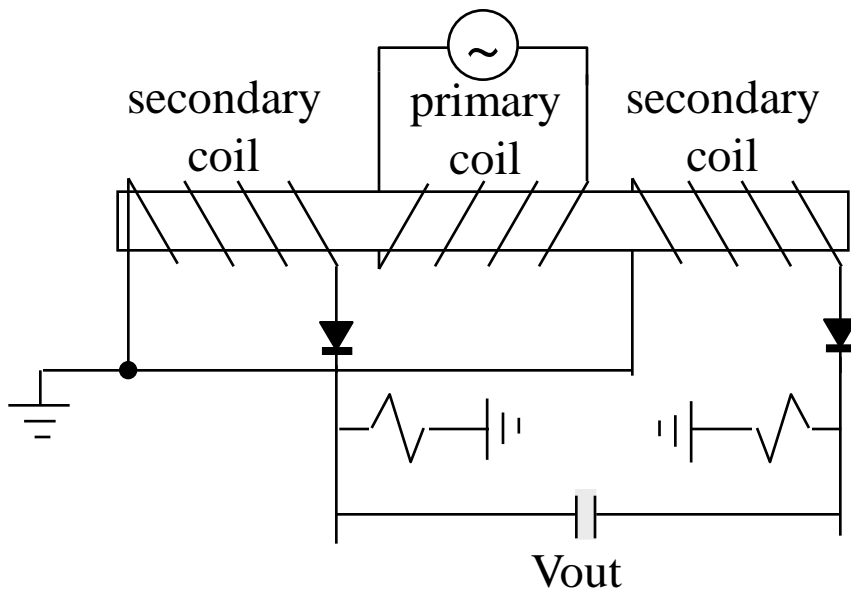
- Thermocouple signal conditioning
 - x100 amplification, susceptible to electrical noise and E/M interference
 - twisted wires, grounded sheath, grounded junction
 - Reference compensation circuits with precision thermistors
- Bimetallic strips (volume expansion)
- Gas thermometer (sensitive but slow)
 - vapor pressure, liquid expansion, solid-state
- Pyrometers (more details in optical sensor section)

Position-Motion Sensors

- Displacement-location-position
 - Ex. liquid level, object position/orientation, infer pressure
 - Potentiometers: resistance and wiper
 - wear, friction, resolution, noise; but linear and simple
 - Capacitance: $C = K\epsilon_0 A/d$
 - ex. movement of one plate changes area; measurement with an AC bridge
 - Inductance: Armature moving through a coil

Position-Motion Sensors

- LVDT: Linear Variable Differential Transformer
 - Key component of many sensors
 - 2 μ m resolution in commercially available systems



moving core

- Difference in secondary coil voltages is linear with displacement.
- Phase shift indicates direction of motion.

Position-Motion Sensors



- Level sensors
 - Float with a secondary displacement measuring system (e.g., LVDT)
 - Based on capacitance or conductivity properties of the fluid
 - Ultrasonic non-contact sensor (measuring reflection time)
 - Pressure-based sensor

Position-Motion Sensors



- Motion types
 - rectilinear motion (v,a), ~10g acceleration
 - angular motion (rotation)
 - vibration, ~100g, $\cos wt \rightarrow w^2 \cos wt$
 - shock (impact), ~500g
- Motion sensors
 - Accelerometers (mass-spring)
 - Natural frequency $f_N = \frac{1}{2\pi} \sqrt{\frac{k}{m}}$

Position-Motion Sensors: accelerometers

- $f < f_N/2.5$: f_N has little effect on response
 - $f > 2.5 f_N$: response independent of applied frequency; a vibration measurement; the “seismic mass” remains roughly stationary
- Potentiometric accelerometers: ~30g, steady-state acceleration, low frequency vibrations
 - LVDT: 80Hz, Variable reluctance (LVDT-like), 100Hz, vibration only, geophones
 - Piezoelectric: 2kHz, shock and vibration apps.

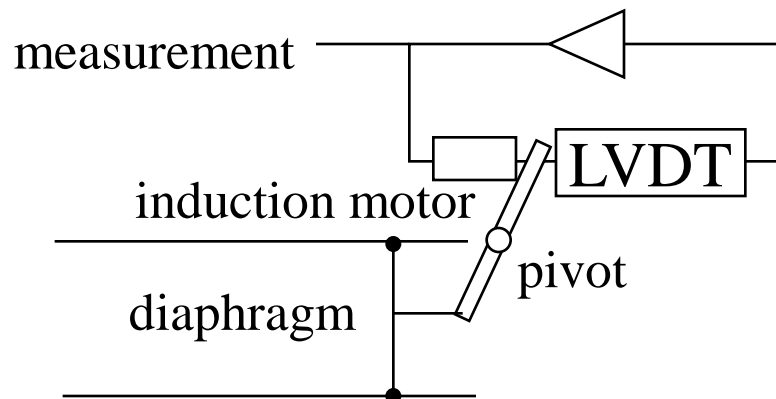
Pressure Sensors



- Pressure basics
 - F/A, units Pa, psi, Atm, bar. (1bar ~ 1atm ~ 100kPa ~ 14.7psi)
 - Static pressure (no flow).
 - Dynamic pressure (flow-dependent)
 - Gauge pressure ($p_{\text{abs}} - p_{\text{atm}}$)
 - Head pressure (ρgh , static)

Pressure Sensors

- Pressure sensors, $>1\text{atm}$
 - with diaphragm or bellows, and LVDT sensor
 - Bourdon tube
 - electronic conversion



Pressure Sensors



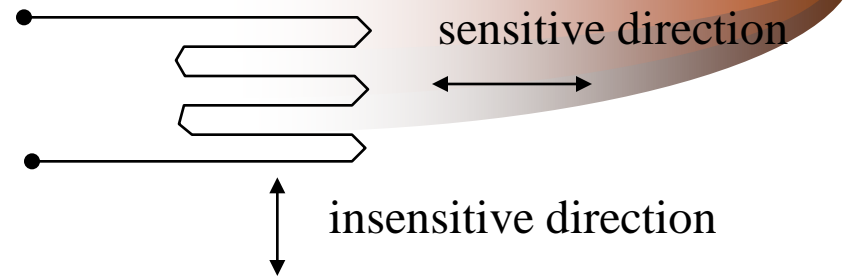
- Pressure sensors, $<1\text{ atm}$ (electronic)
 - Pirani gauge. Filament temperature via resistance measurement or thermocouple-based; nonlinear pressure dependence); 10^{-3} atm , calibrated for the type of gas.
 - Ionization gauge 10^{-3} - 10^{-13} atm
 - heated filament - electrons - ionized gas - current between electrodes
 - approximately linear

Strain Sensors

- Stress = F/A ; tensile, compressional, shear
- Strain = $\Delta l/l$; tensile, compressional, shear
- Modulus of elasticity (Young) $E = \text{stress/strain}$
 - linear for low stress, elastic region
- Strain gauge: resistance change \sim strain
 - order of 0.1% fractional change
 - temperature compensation necessary (temperature effects are more significant)

Strain Sensors

- Wire/foil gauges
- Semiconductor gauges
- Gauge Factor = $\frac{\Delta R/R}{strain}$
 - 2 - 10 for metals
 - (-5) - (-200) for semiconductors but nonlinear
- Applications
 - load cells for large weight measurement (~500tons)
 - force sensors for nonlinear feedback in robotics



Flow Sensors



- Conveyor belt
 - load cell with strain gauge: measure weight on a fixed length of belt; belt speed is given/measured
- Liquid (volume or mass flow)
 - restriction (Venturi, orifice plate, nozzle) $Q \sim k\sqrt{\Delta p}$
 - obstruction: rotameter (liquid/gas), moving vane (angle~flow), turbine (tachometer~flow)
 - magnetic, (conductors/insulated pipe): flow through a magnetic field and measure the transverse potential

Optical Sensors



- EM radiation spectrum

| Band | Frequency | Wavelength $c = \lambda f$ |
|-----------|--------------|-------------------------------|
| VLF | MHz | 300m |
| TV/radio | MHz-GHz | 0.3m |
| Microwave | THz | 0.3mm |
| Infrared | 10^{15} Hz | 0.3um |
| Visible | | 400-760nm |
| UV | 10^{17} Hz | 3nm |

Optical Sensors



- Photo detectors
 - spectral response (wavelengths)
 - time-constant, response time
 - detectivity
- Photo conductive detectors
 - semiconductor conductivity (or resistance) as a function of radiation intensity
 - resistance drops as number of absorbed photons with higher energy than band gap increases

Optical Sensors

- temperature control is important since it affects resistance

| Photo-conductor | time constant | spectral band |
|-----------------|---------------|-----------------|
| CdS | 100ms | 0.47-0.71 μ |
| CdSe | 10ms | 0.6-0.77 μ |
| PbS | 400 μ s | 1-3 μ |
| PbSe | 10 μ s | 1.5-4 μ |

Optical Sensors



- Photo Voltaic detectors
 - “giant diodes”, $V = V_o \log(I)$
 - time-constants: Si (20us), Se (2ms), Ge (50us), InAs (1us)
 - photodiode detectors (changes in I-V characteristics): 1us - 1ns response time (for communication apps)
 - photoemissive detectors: current \sim light intensity, photo-multipliers, very sensitive

Optical Sensors



- Pyrometers
 - Temperature \sim emitted EM radiation; black body radiation $\sim T^4$ (total)
 - Broadband pyrometers, total radiation pyrometers
 - micro-thermocouple on blackened Pt disc; heats up with radiation and thermocouple generates a voltage; responds to all wavelengths
 - IR pyrometer (Si-Ge)

Optical Sensors



- Pyrometer applications
 - Metal production, glass production, semiconductors
 - range 0-1000°C
 - accuracy 0.5-5°C
 - noninvasive
 - Correction factors
 - Contamination issues (viewport fogging)

Optical Sensors



- Optical light sources
 - conventional: incandescent, atomic (distributed, divergent, incoherent, polychromatic)
 - Laser (monochromatic, coherent, non-divergent)

| | | | |
|-----------------|-------|----------------------|-----------------------------------|
| He-Ne | red | 0.5-100mW (cont) | ranging alignment, comm. |
| Ar | green | 0.1-5W (cont) | heat, small welding, comm. |
| CO ₂ | IR | 1-100kW (cont-pulse) | cutting, welding, drilling, comm. |
| Ruby | red | 1GW (pulse) | cutting, welding, drilling, comm. |

Optical Sensors

- Incremental Optical encoders
 - Identical, equally spaced transparent windows
 - Two photodiodes, quarter pitch apart (to establish direction).
 - Angle of rotation is the summation of pulse counts (rising edge).
 - Velocity is window spacing by elapsed time.
 - Resolution is: $\Delta\theta = \frac{2\pi}{N}$, $\Delta\omega = \frac{2\pi}{NT}$ N = windows, T = sampling time
 - e.g., 10,000 windows \Rightarrow 0.018° resolution

Optical Sensors



- Absolute Optical encoders
 - Code pattern on the encoder disk
 - N tracks to provide 2^N resolution ($N \sim 14$), each track associated with a pick-off sensor
 - Gray coding: one bit switching between adjacent sectors; minimizes errors due to manufacturing tolerances (e.g., eccentricity)

Actuators and Final Control Elements



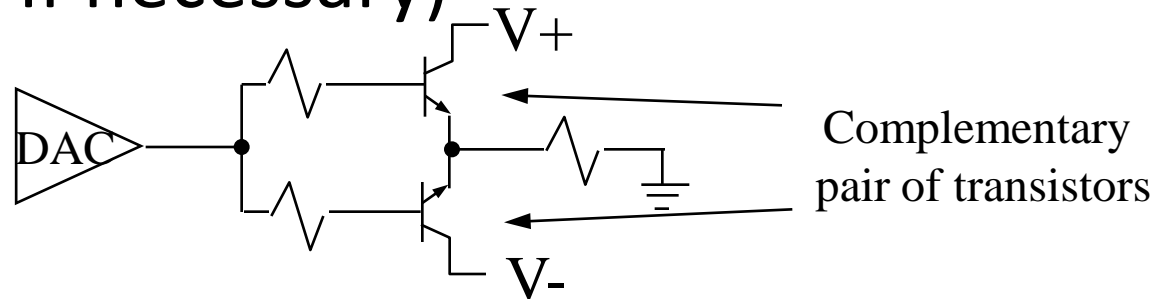
- Implementing changes in process variables
 - Relays, SCR/TRIAC (motor and heater control)
 - Amplifiers (Analog, PWM)
 - Solenoids (electromechanical conversion)
 - coil and plunger; free standing or spring loaded
 - Motors
 - DC: series field (hi-torque, difficult speed control); shunt (lower torque, easy speed control); compound
 - AC (Synchronous-Asynchronous, Low starting torque)
 - Stepping

Actuators and Final Control Elements

- Pneumatic signals: pressure as information carrier
 - 3-15psi standard , 330m/s propagation (sound)
- Amplifiers (diaphragm-based), Hydraulics
 - Nozzle-Flapper (mechanical-pneumatic conversion)
 - Diaphragm-Spring (pneumatic-mechanical conversion)
 - Current-2-Pressure conversion (solenoid-nozzle-flapper)
- Valves (Quick open, Linear, Equal Percentage)
- Hopper valves (solids), Rollers

Actuators

- Push-pull class B amplifier. (Use multiple stages, if necessary)

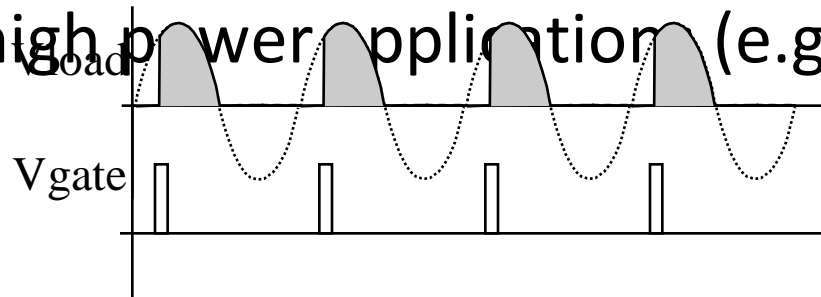


- Pulse Width Modulated (PWM) amplifiers
 - Varying the duty cycle of a square wave
 - Efficient switching transistors for high power requirements

Actuators

- Silicon-Controlled Rectifier (SCR, thyristor)
 - trigger voltage at the gate will start conducting positive voltages from anode to cathode; it will stop when the forward bias at the gate is off and the anode voltage is negative (half-wave operation)
 - TRIAC: full-wave operation
 - Power Control for high power application (e.g., heating)

SCR
half-wave
operation



Bibliography



- Curtis Johnson, *Process Control Instrumentation Technology*, 4th ed. Prentice Hall, New Jersey 1993.
- Lennart Ljung, *System Identification: Theory for the User*. Prentice Hall,